Contains nonbinding recommendations

Decision Tree 2 provides an approach for setting specifications for polymorphs in the drug substance when at least one form is known to have low solubility based on the BCS. If relevant and adequate specifications for polymorphs are included in the USP, ANDA applicants may adopt these specifications for the drug substance polymorphic form. Otherwise, we recommend that a new specification for the drug substance polymorphic form be established.

C. Investigating the Importance of Setting Specifications for Polymorphs in Drug Products

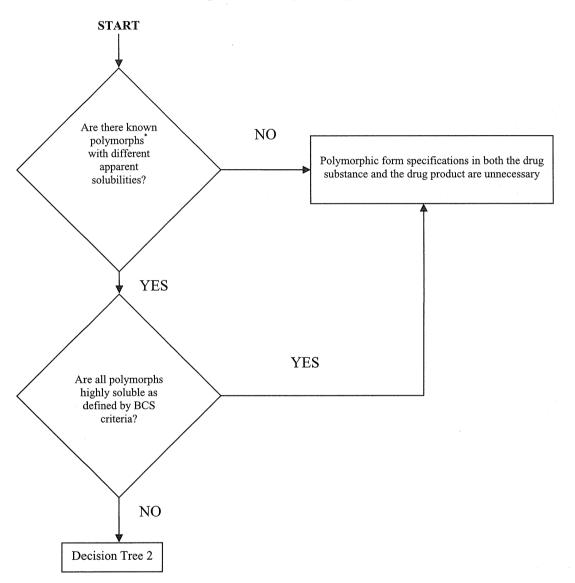
Decision Tree 3 provides an approach when considering whether to set specifications for polymorphs in the drug product. Generally, specifications for polymorphs in drug products are not necessary if the most thermodynamically stable polymorphic form is used or if the same form is used in an approved product of the same dosage form. However, since manufacturing processes can affect the polymorphic form, we recommend that you use caution if a metastable form is used.

Drug product performance testing (e.g., dissolution testing) can also generally provide adequate control of polymorph ratio changes that can influence drug product BA/BE for poorly soluble drugs. In such instances, setting specifications for polymorphs in the drug product would generally not be considered important for ensuring adequate product performance. Only in rare cases would we recommend setting specifications for polymorphic forms in drug products.

ATTACHMENT 1 - DECISION TREE 1

Decision Tree 1

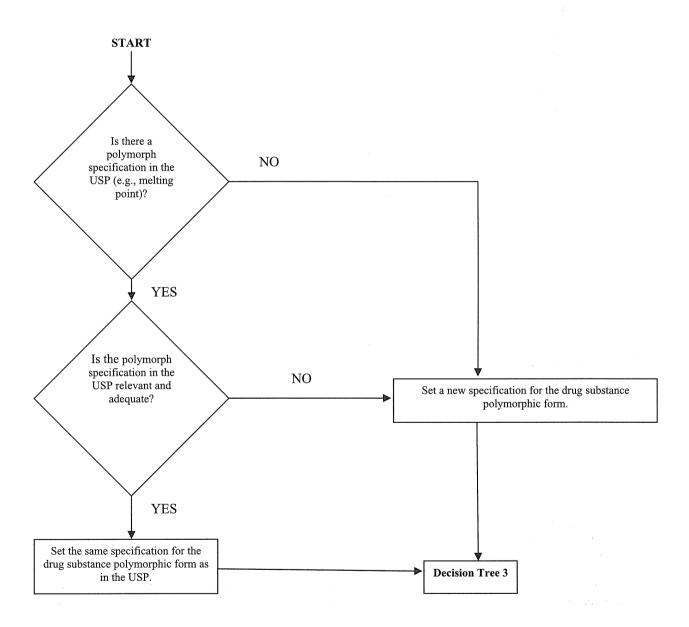
Investigating whether to set specifications for polymorphs for solid oral and suspension dosage form products.



^{*}We recommend that you consider only those polymorphs that are likely to form during manufacture of the drug substance, manufacture of the drug product, or while the drug substance or drug product is in storage. See footnote 7 in this guidance document.

ATTACHMENT 2 – DECISION TREE 2

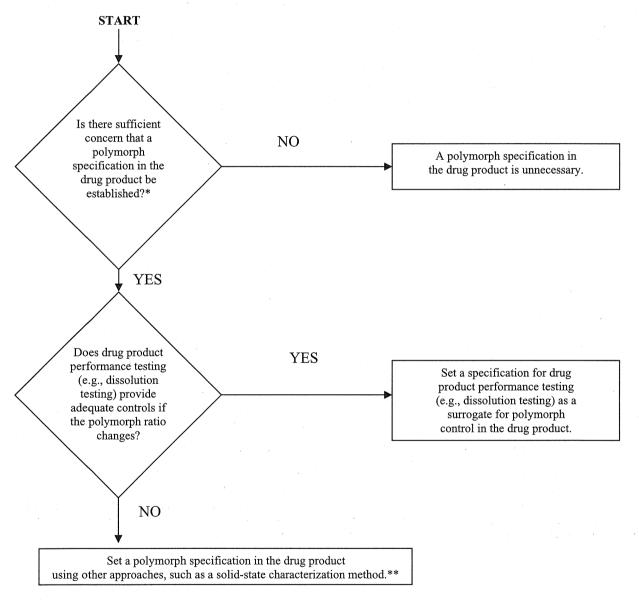
Decision Tree 2 Setting specifications for polymorphs in drug substances for solid oral and suspension dosage form products.



ATTACHMENT 3 – DECISION TREE 3

Decision Tree 3

Investigating whether to set specifications for polymorphs in drug products for solid oral and suspension dosage form products.



^{*}In general, there may not be a concern if the most thermodynamically stable polymorphic form is used or the same form is used in a previously approved product of the same dosage form.

^{**}Drug product performance testing (e.g., dissolution testing) can generally provide adequate control of polymorph ratio changes for poorly soluble drugs, which may influence drug product BA/BE. Only in rare cases would polymorphic form characterization in the drug product be recommended.

別添資料2

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5.9. POLYMORPHISM

Polymorphism (or crystal polymorphism) is a phenomenon related to the solid state; it is the ability of a compound in the solid state to exist in different crystalline forms having the same chemical composition. Substances that exist in a non-crystalline solid state are said to be amorphous.

When this phenomenon is observed for a chemical element (for example, sulphur), the term allotropy is used instead of polymorphism.

The term pseudopolymorphism is used to describe solvates (including hydrates), where a solvent is present in the crystal matrix in stoichiometric proportions; the term may also be extended to include compounds where the solvent is trapped in the matrix in variable proportions. However the term pseudopolymorphism is ambiguous because of its use in different circumstances. It is therefore preferable to use only the terms "solvates" and "hydrates".

Where a monograph indicates that a substance shows polymorphism, this may be true crystal polymorphism, occurence of solvates, allotropy or occurrence of the amorphous form.

The identity of chemical composition implies that all crystalline and amorphous forms of a given species have the same chemical behaviour in solution or as a melt; in contrast, their physico-chemical and physical characteristics (solubility, hardness, compressibility, density, melting point, etc.), and therefore their reactivity and bioavailability may be different at the solid state.

When a compound shows polymorphism, the form for which the free enthalpy is lowest at a given temperature and pressure is the most thermodynamically stable. The other forms are said to be in a metastable state. At normal temperature and pressure, a metastable form may remain unchanged or may change to a thermodynamically more stable form.

If there are several crystalline forms, one form is thermodynamically more stable at a given temperature and pressure. A given crystalline form may constitute a phase that can reach equilibrium with other solid phases and with the liquid and gas phases.

If each crystalline form is the more stable within a given temperature range, the change from one form to another is reversible and is said to be enantiotropic. The change from one phase to another is a univariate equilibrium, so that at a given pressure this state is characterised by a transition temperature. However, if only one of the forms is stable over the entire temperature range, the change is irreversible or monotropic.

Different crystalline forms or solvates may be produced by varying the crystallisation conditions (temperature, pressure, solvent, concentration, rate of crystallisation, seeding of the crystallisation medium, presence and concentration of impurities, etc.).

The following techniques may be used to study polymorphism:

- X-ray diffraction of powders,
- X-ray diffraction of single crystals,
- thermal analysis (2.2.34) (differential scanning calorimetry, thermogravimetry, thermomicroscopy),
- microcalorimetry,
- moisture absorption analysis,
- optical and electronic microscopy,
- solid-state nuclear magnetic resonance,
- infrared absorption spectrophotometry (2.2.24),
- Raman spectrometry (2.2.48),
- measurement of solubility and intrinsic dissolution rate,
- density measurement.

These techniques are often complementary and it is indispensable to use several of them.

Pressure/temperature and energy/temperature diagrams based on analytical data are valuable tools for fully understanding the energetic relationship (enantiotropism, monotropism) and the thermodynamic stability of the individual modifications of a polymorphic compound.

For solvates, differential scanning calorimetry and thermogravimetry are preferable, combined with measurements of solubility, intrinsic dissolution rate and X-ray diffraction.

For hydrates, water sorption/desorption isotherms are determined to demonstrate the zones of relative stability.

In general, hydrates are less soluble in water than anhydrous forms, and likewise solvates are less soluble in their solvent than unsolvated forms.

別紙4

研究成果の刊行

書籍

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Relationship between Crystallization Tendencies during Cooling ₂ from Melt and Isothermal Storage: Toward a General Understanding 3 of Physical Stability of Pharmaceutical Glasses

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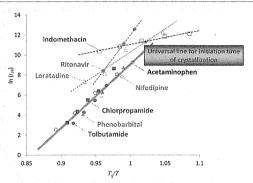
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ABSTRACT: The lack of protocols to predict the physical stability has been one of the most important issues in the use of amorphous solid dispersions. In this paper, the crystallization behaviors of pharmaceutical glasses, which have large variations in their crystallization tendencies, have been investigated. Although each compound appears to have a wide variation in their crystallization time, the initiation time for crystallization could be generalized as a function of only T_g/T , where T_g and T are the glass transition temperature and storage temperature, respectively. All compounds in which crystallization was mainly governed by temperature had similar activation energies for crystallization initiation, ca. 210-250 kJ/ mol, indicating that physical stability at any temperature is predictable from only $T_{\rm g}$. Increased stability is expected for other compounds, where crystallization is inhibited by an large energetic barrier, and stochastic



nucleation plays an important role in initiating crystallization. The difference in the dominant factor, either temperature or pressure, appeared to correlate with the nucleation mechanism, and this could be determined by a cool-heat cycle after melting using thermal analysis. This conclusion should make prediction of physical stability of amorphous formulations easier, although the investigation was conducted under ideal conditions, which eliminated surface effects.

KEYWORDS: amorphous, crystallization, nucleation, glass transition temperature, activation energy, stability prediction 29

30 INTRODUCTION

31 Amorphous solid dispersion is one of the most important 32 formulation technologies for poorly soluble drugs because it 33 can improve the dissolution process and, therefore, their 34 bioavailability. 1-4 However, although amorphization is regarded 35 as a conventional technology for injectable formulations, the 36 number of marketed oral amorphous formulations is still 37 limited. One of the major concerns for the use of amorphous 38 forms has been their physical stability. 3,4 In most cases, 39 injectable formulations are under the control of medical 40 personnel. However, oral formulations are usually handled by 41 patients, and the stability requirements are more severe. In 42 addition, amorphization technology is frequently applied to 43 peptide drugs in the case of injectable formulations, of which 44 the intrinsic crystallization tendency is very low. From the 45 viewpoint of developmental studies, the lack of an accelerated 46 study protocol for predicting the crystallization behavior of 47 amorphous forms has been an issue that inhibits their wide 48 use.^{3–5}

Many attempts have been made to derive a general rule that 49 determines the crystallization tendency of organic compounds. 50 Requirements for chemical structures of good glass formers 51 have been indicated, e.g., a large molecular weight with a low 52 number of benzene rings, low level of molecular symmetry, 53 many rotatable bonds, branched carbon skeletons, and 54 electronegative atoms. ⁶⁻⁸ Also, good glass formers tend to 55 have a large enthalpy/entropy of fusion, large free energy 56 difference between crystalline and amorphous states, and high 57 melting temperatures.⁷ Interactions between the molecules and 58 molecular mobility are also important factors. 9,10 Fragility, 11,12 59 which is a measure of the non-Arrhenius characteristics of 60 liquids/glasses, is another factor that is thought to influence 61 crystallization ability. 7,13 However, although these factors have 62 been shown to correlate with the glass forming ability to some 63

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Table 1. List of Model Drugs Used in This Study

classification ^a	compound	abbreviation	$M_{ m w}$	$T_{\rm m}$ (°C) ^b	$T_{g} (^{\circ}C)^{c}$	supplier
I	chlorpropamide	CPA	276.7	122	16	Sigma-Aldrich (St. Louis, USA)
	haloperidol	HPD	375.9	150	27 ^d	Nacalai Tesque (Kyoto, Japan)
	tolbutamide	TLB	270.3	128	5	Wako Pure Chemicals (Osaka, Japan)
II	acetaminophen	AAP	151.2	169	24	MP Biomedicals (Santa Ana, USA)
	nifedipine	NDP	346.3	173	46	Alexis Biochemicals (San Diego, USA)
III.	Ioratadine	LTD	382.9	135	38	Tokyo Chemical Industry (Tokyo, Japan)
	ritonavir	RTV	721.0	127	47	LKT Laboratories (St. Paul, USA)
_			, <i>L</i>			

^aClassification system introduced by Taylor et al. (see text). ^bPeak temperature. ^cOnset temperature. ^dDetermined by high-speed DSC.

64 extent, they do not provide quantitative information on the 65 crystallization behavior of a specific compound. Representative 66 examples of quantitative measures of glass-forming ability are 67 the reduced glass transition temperature, which is a ratio of 68 glass transition and melting temperatures, and onset cold 69 crystallization temperature. 14 However, these investigations 70 have mainly been made on metallic alloys, and there are few 71 such observations for organic compounds. Ping et al. 72 investigated the glass-forming ability of o-terphenyl and 73 structurally related compounds and concluded that compounds 74 with high reduced glass transition temperatures (above 0.73) 75 were good glass formers, while those with low reduced glass 76 transition temperatures (below 0.68) were poor glass formers. 15 This knowledge has been developed mainly from observa-78 tions of crystallization behavior during cooling from the melt. It 79 does not provide direct information on the isothermal 80 crystallization behavior, which is of great interest for 81 formulators. Dynamics of molecules, which should have a 82 great impact on the crystallization behavior, are influenced by 83 both thermal energy (temperature) and molecular packing 84 (pressure/volume). ^{16,17} Both factors are continuously changing 85 and have a significant impact on the crystallization process 86 during cooling, while basically, isothermal crystallization should 87 rely on fluctuations in the local energy to break the energetic 88 barrier of crystallization, although the free energy change 89 accompanied by crystallization is essentially the same for both 90 types of processes. Presented here is an observation of the 91 isothermal crystallization behaviors of model compounds, 92 which have various crystallization tendencies during cooling 93 from the melt and subsequent reheating. The relationship 94 between the crystallization behavior and their dominating 95 factor, either temperature or pressure, is discussed. A simple 96 prediction protocol for physical stability is also provided.

97 MATERIALS AND METHODS

Materials. All the model drugs used in this study are listed 99 in Table 1 with their supplier, abbreviation, and basic 100 characteristics. All compounds were used as supplied.

Differential Scanning Calorimetry (DSC). DSC measurements were performed on a DSC Q2000 (TA Instruments, 103 New Castle, DE, USA), which were periodically calibrated 104 using indium and sapphire. Dry nitrogen was used as the inert 105 gas at a flow rate of 50 mL/min. Crimped aluminum pans were 106 used for the measurements except in the case of nifedipine 107 (NDP), for which hermetic aluminum pans were used, because 108 sorption of a trace amount of moisture during handling 109 dramatically influenced its crystallization. All evaluations were 110 at least performed in triplicate. Heat capacity measurements 111 were performed in the modulated DSC mode using the

protocol established previously¹⁸ in which the sample (ca. 10 112 mg) was heated in a crimped T-zero aluminum pan at 2 °C/ 113 min with a 60 s period and 0.5 °C amplitude. Amorphous 114 samples were prepared by quenching at 50 °C/min from above 115 the melting temperature. Although accuracy of this cooling rate 116 was not assured by the manufacturer of the instrument, it was 117 confirmed to be successfully achieved according to the 118 temperature data.

X-ray Powder Diffraction (XRPD). XRPD patterns were 120 acquired on a Rigaku RINT Ultima X-ray diffraction system 121 (Rigaku Denki, Tokyo, Japan) using Cu K α radiation. The 122 voltage and the current were 40 kV and 40 mA, respectively. 123 Data were collected between 3° and 40° (2 θ) at intervals of 124 0.02° with a scan speed of 2°/min.

lsothermal Annealing. After quenching in the DSC, all the 126 glass samples were subjected to annealing at various temper-127 atures. Annealing shorter than 48 h was performed in DSC. 128 When longer annealing was required, the samples in the DSC 129 pans were stored in desiccators with silica gel in temperature-controlled ovens. The difference in the storage protocol was 131 negligible for all the compounds.

Synchrotron Wide-Angle X-ray Diffraction (WAXD). 133
Simultaneous measurements of WAXD/DSC were performed 134
at BL40B2 of the synchrotron facility SPring-8 (Sayo, Japan). 135
The wavelength of the incident X-ray beam was 0.100 nm. A 136
Hamamatsu flat panel (50um/pixel) was used as the 2D 137
detector for WAXD measurements and the sample-to-detector 138
distance was 53.9 mm, which was calibrated using silver 139
behenate. The exposure time was 1 s. The WAXD image was 140
displayed using LabView software ImageView92. Exothermic 141
heat flow due to crystallization of tolbutamide (TLB) and 142
acetaminophen (AAP) was observed with Thermo Plus DSC 143
(Rigaku, Tokyo, Japan). TLB was melted at 140 °C, followed 144
by cooling at 5 °C/min. AAP was melted at 200 °C, followed 145
by cooling at 30 °C/min to 0 °C and reheating at 5 °C/min. 146

Thermal Stability of Model Compounds. The thermal 147 stability of each drug was investigated using thermogravimetric 148 (TG) analysis on SDT Q600 (TA Instruments, New Castle, 149 DE, USA) and high-performance liquid chromatography 150 (HPLC). TG analysis was performed up to the melting 151 temperatures to observe weight loss due to decomposition and 152 sublimation. The compounds that exhibited weight loss more 153 than 0.01% in the TG study were subjected to HPLC analysis 154 on a Shimadzu Prominence (Shimadzu, Kyoto, Japan) 155 equipped with a Cosmosil 5C18-AR-II (150 mmL × 5.0 156 mmID, Nacalai Tesque, Kyoto, Japan) with a flow rate of 1 157 mL/min. The column was equilibrated by acetonitrile/water = 158 5/95, and measurements were done with this mobile phase for 159 10 min, followed by a gradual change to 100/0 over 40 min and 160

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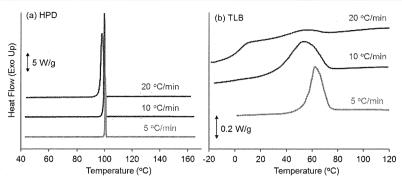


Figure 1. DSC cooling curves of the class I compounds from the melt. 17 The cooling rates are indicated.

 $_{161}$ elution by acetonitrile for 10 min. The detection wavelength $_{162}$ and injection volume were 210 nm and 2 μL , respectively. $_{163}$ Some compounds exhibited weight loss at very low temperature $_{164}$ (<100 °C), followed by flat baselines. In such cases, the weight loss was interpreted as removal of adsorbed water, and only the $_{166}$ weight loss after the flat baseline was evaluated.

The Classification System. The basic idea ("protocol for los classification") for the classification system presented below was introduced by Taylor et al., which was established by observing the crystallization behavior during cooling from the melt and subsequent reheating. Their purpose was classification of the compounds on the basis of crystallization tendency during the cooling and reheating, and the origin of different crystallization behaviors was not discussed in detail. We have added our interpretation of the dominant factor in the crystallization process, that is, either temperature or pressure, based on the investigation of the cooling rate-dependence of the crystal-investigation temperature, as described next.

179 Class I: Crystallization is dominated by thermodynamics.
180 Temperature (degree of supercooling) is a dominant factor for
181 controlling the crystallization process. Protocol for classifica182 tion: Compounds that crystallized during cooling from the
183 melt at 20 °C/min.

184 Class II: Crystallization is influenced by competition between 185 thermodynamic and kinetic factors. Basically temperature 186 dominates crystallization; however, the transformation is 187 disturbed by steric hindrance (local pressure).

Protocol for classification: Compounds that do not crystallize during cooling from the melt at 20 $^{\circ}$ C/min but crystallize during subsequent reheating at 20 $^{\circ}$ C/min.

Class III: Crystallization is dominated by pressure. Stochastic nucleation plays a dominant role in controlling the crystal-193 lization process.

Protocol for classification: Compounds that do not crystallize during the cooling/reheating cycle presented above.

An amorphous state is thermodynamically unstable and always seeks opportunities to transform into a crystalline state. The initial nucleation step is a trigger for this transformation. If the energetic barrier for nucleation is very small, basically due to a small steric hindrance, crystallization should be controlled to by the free energy difference between the crystalline and amorphous states, which can be described as a function of only temperature under ambient pressure condition. This is a situation where the system is thermodynamically (temperature) controlled (class I). If the melt is cooled from the melting temperature, crystallization should occur at the same temperature regardless of the cooling rate in this case. Homogeneous nucleation may be expected because no templates are required.

In contrast, the free energy difference is less important if the 209 energetic barrier for the nucleation is large enough. In this case 210 where probability of nucleation is very low, the transformation 211 relies on local thermal and density fluctuations to induce 212 "stochastic" nucleation. Once the nuclei are formed, crystal 213 growth should follow, using the nuclei as templates. This 214 "pressure-controlled" situation should be initiated by hetero- 215 geneous nucleation, and crystallization during cooling and 216 reheating is not likely to occur (class III). If there is a moderate 217 energetic barrier for nucleation, crystallization may occur 218 during the cooling and reheating cycle. The cooling rate 219 should have a significant impact on the crystallization 220 temperature because it influences the frustration in the 221 molecular structure that determines the energetic barrier for 222 nucleation (class I or II).

Figure 1 shows DSC cooling curves from the melt for 224 ft haloperidol (HPD) and TLB, ¹⁹ both of which are classified as 225 class I compounds. HPD always crystallized at 100 °C 226 regardless of the cooling rate. The crystallization of HPD is 227 clearly dominated by temperature, because if the kinetic factor 228 influenced the crystallization process, the crystallization 229 temperature should depend on the cooling rate. Such cooling 230 rate-insensitive crystallization can be found for many class I 231 compounds including atenolol, benzamide, caffeine, and 232 indoprofen. TLB also crystallizes during the cooling scan; 233 however, the crystallization temperature depends on the 234 cooling rate. Moreover, only partial crystallization was observed 235 when TLB was cooled at 20 °C/min, and glass transition 236 behavior was also detected at 3 °C. Thus, crystallization of TLB 237 seemed to be dominated by temperature but there was also a 238 kinetic contribution. When TLB was cooled at 50 °C/min, it 239 failed to crystallize in the cooling process but crystallized in the 240 subsequent reheating. Thus, while both class I and II 241 compounds are mainly controlled by temperature, there is a 242 difference in the relative contribution of thermodynamic and 243 kinetic factors in the crystallization process. Theoretically, class 244 III compounds should crystallize as well if they are cooled or 245 reheated at a very slow scan rate, but this was found to be 246 practically impossible.

RESULTS AND DISCUSSION

Thermal Stability of Model Compounds. In the 249 following experiments, each drug was melted before assessment 250 of crystallization behavior and heat capacity measurement. If 251 decomposition occurs, it can influence the crystallization rate 252 significantly. All the compounds used in this study were 253 confirmed to be stable during the 1 min melting. Thus, the 254 melt—quench procedure did not seem to produce degradation 255

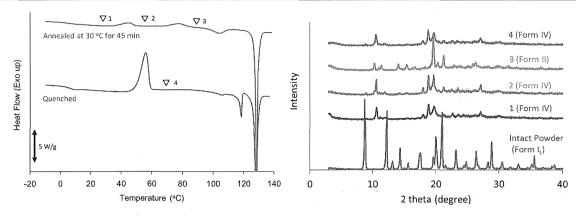


Figure 2. (left) DSC heating curves (10 °C/min) of quenched and annealed TLB. The quench was done in the DSC at a cooling rate of 50 °C/min. The annealing was also performed in the DSC at 30 °C for 45 min. The XRPD patterns of the samples at the indicated point (1–4) on the DSC curves are presented on the right with assignment of the crystal forms. (right) The XRPD patterns of the samples collected from the DSC pan. The DSC measurements were terminated at the indicated point in the left figure for supplying the samples to the XRPD analysis. The sample weight for this purpose was larger than 10 mg.

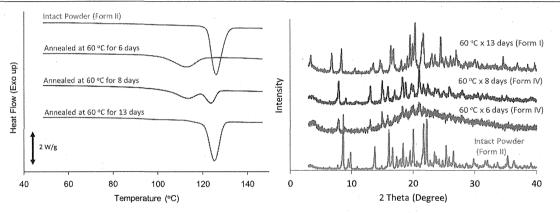


Figure 3. (left) DSC heating curves (10 °C/min) of annealed RTV after the quenching. The annealing was done at 60 °C in a temperature-controlled oven for the indicated period. (right) The XRPD patterns of the annealed RTV at 60 °C for the indicated period with assignment of the crystal forms.

256 products. Most of the compounds were also stable during the 257 storage performed in this study. However, ritonavir (RTV) 258 produced approximately 5% of degradation products during 259 storage at 60 °C for 1 month. Although no degradation 260 products were detected for loratadine (LTD) after 1 month of 261 storage at 60 °C, the sample was slightly red in color, which 262 obviously indicated degradation. However, crystallization of 263 both RTV and LTD was almost completed in one month at 60 264 °C. This study focuses on the 10% crystallization time, which 265 was completed in 3 days and 1 day for RTV and LTD, 266 respectively, for which impact of degradation was negligible.

Determination of Crystallinity. The crystallinity of class I and II compounds was determined from the crystallization enthalpy observed during the heating process in DSC measurements, except for NDP. Figure 2 shows the DSC rowstallized to form IV at ca. 50 °C in the heating process, revealed by the XRPD analysis and an exothermic enthalpy of gradually crystallized to form IV. Figure 2 also shows the parallel gradually crystallized to form IV. Figure 2 also shows the remaining curve of TLB, which was stored at 30 °C for 45 min. It exhibited a small exothermic peak at ca. 40 °C, which was due to crystallization of the remaining amorphous part to form IV.

It transformed to form II at ca. 80 $^{\circ}$ C, and to form I_h (high- 279 temperature stable form of form I) at ca. 100 $^{\circ}$ C. The 280 crystallinity, X, of the stored sample can be calculated as 281 follows.

$$X(\%) = 100\{\Delta H/(\Delta H_{q} - \int_{T}^{T_{q}} \Delta Cp)\}$$
 (1) ₂₈₃

where ΔH and $\Delta H_{
m q}$ are the crystallization enthalpies of the 284 annealed and quenched (i.e., no annealing) samples, 285 respectively. T and T_q are the crystallization temperatures, 286 and peak temperatures were used for simplicity. ΔC_p is the heat 287 capacity difference of the amorphous and crystalline forms 288 obtained by temperature-modulation measurements. The 289 integration term was calculated numerically. In a similar 290 procedure, crystallinity of the recrystallized quenched sample 291 was proved to be almost 100%. Form I_h melt temperature is at 292 127 °C with a melting enthalpy of ca. 106 J/g. Heat capacity 293 difference between forms I and IV were negligible, and they 294 exhibited lower values than that of supercooled liquid by ca. 295 0.45 J/g. Because the temperature difference between melting 296 of form I_h and crystallization to form IV was approximately 77 297 °C, expected crystallization enthalpy of form IV is 71 J/g, which 298 almost agrees with the observed value, 72 J/g.

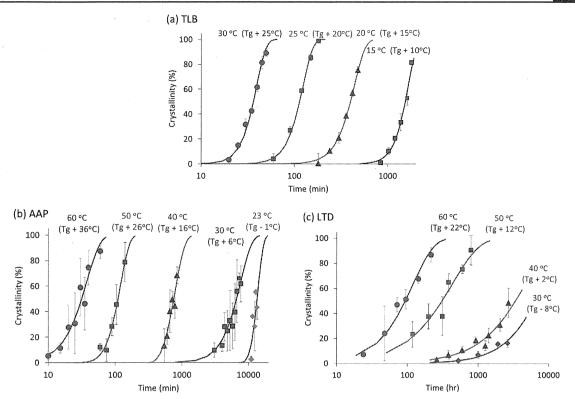


Figure 4. Evolution of crystallinity of the quenched TLB, AAP, and LTD as a function of time at the indicated temperature. The annealing was made either in DSC (≤24 h) or temperature-controlled ovens (>24 h). Consistency of the two annealing procedures was confirmed for some samples. Each measurement was at least triplicated for showing error bars as standard deviations. The fitting lines were drawn based on the Avrami−Erofeev equation.

The crystallinity of chlorpropamide (CPA) and AAP (crystallization to form III) was calculated by the same procedure with that for TLB. Although NDP crystallized in the same manner during heating, an exothermic transformation peak just after the crystallization inhibited integration of the peak because of their overlap. Thus, a shift in the baseline due to partial crystallization was used to estimate the crystallinity, which can be described by the following equation.

$$X(\%) = 100(W - W_a)/\Delta W$$
 (2)

309 where W and W_a are the heat flows of the annealed sample and 310 amorphous reference, which were obtained by cooling and 311 subsequent reheating after measurement of the annealed 312 sample. This equation is based on the fact that the crystalline 313 and amorphous states have their own heat capacities which 314 allow for determination of crystallinity by measuring the heat 315 capacity of the sample of interest. Due to the partial 316 crystallization, the heat capacity of the annealed sample was 317 between the heat capacities of crystalline and amorphous 318 samples, depending on the crystallinity. Because W and W_a are 319 functions of temperature, the values were read at the parallel 320 part of the heating curves between $T_{\rm g}$ and the crystallization 321 temperature, typically at 60 °C in the case of NDP. ΔW is the 322 difference in the heat flow between amorphous and crystalline 323 samples, for which the value of 0.0785 W/g was applied. 324 Theoretically, this method should be applicable to any 325 compounds and was confirmed to provide the same crystallinity 326 values for TLB and AAP. However, measurement of the correct 327 heat capacity requires very good thermal contact of the sample with the bottom of the DSC pan. ¹⁸ The samples used in this ³²⁸ study met this requirement because they were prepared by ³²⁹ melt—quenching; however, it is not recommended to apply this ³³⁰ method to powder samples because of their poor thermal ³³¹ contact.

The crystallinity for RTV and LTD was calculated from the 333 melting enthalpy because crystallization did not occur during 334 the heating process. Figure 3 shows DSC curves of the 335 f3 annealed RTV samples at 60 °C and intact crystal (form II). 336 The RTV glass crystallized to form IV initially, followed by 337 transformation to form I after annealing for 7 days. 338 Crystallization to form IV was analyzed in this study. Some 339 samples were still in form IV even after 7 days; however, those 340 samples were excluded from the analysis because inclusion of 341 that data would result in a focus on the slow-crystallization 342 samples. The same crystallization/transformation pattern was 343 observed for samples annealed at 50 °C, where the trans- 344 formation was initiated after annealing for 70 days. Although we 345 did not observe this transformation at 45 °C at least for 9 346 months, it is expected that after sufficiently long storage it will 347 occur because forms I and IV are monotropically related. The 348 crystallinity, X, was calculated using the following equation.

$$X(\%) = 100 \left(\frac{H_{\rm m}}{H_{\rm mi}} \right) \left(\frac{H_{\rm m-II}}{H_{\rm m-IV}} \right)$$
(3) 350

where $H_{\rm m}$, $H_{\rm m}$, $H_{\rm m-II}$, and $H_{\rm m-IV}$ are the melting enthalpies of 351 the annealed sample, the sample before the quenching, form II 352 (87.8 J/g), and form IV (59.8 J/g), ²⁰ respectively. 353

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E

LTD crystallized to a stable form below 30 °C ($T_{\rm m}=135$ 355 °C), while it crystallized to the metastable form above 50 °C 356 ($T_{\rm m}=133$ °C).

Analysis of the Crystallization Process. Figure 4 shows stallization curves of model compounds annealed under various temperature conditions. Each data set was fitted using the Avrami–Erofeev equation as shown below.

$$X(\%) = 100[1 - \exp\{-k(t-d)^n\}]$$
 (4)

 362 where k and d are the crystallization rate constant and 363 induction time, respectively. n is an Avrami exponent, which is 364 determined by the dimension of the crystal growth and 365 nucleation mechanism. TLB exhibited very high reproducibility 366 in its crystallization behavior, as demonstrated by the small 367 error bars for each data point; this is presumably because 368 crystallization is basically governed by thermodynamics. The 369 same trend was observed for another class I compound, CPA. 370 AAP and NDP are class II compounds, and RTV and LTD are 371 class III compounds. Obviously, reproducibility of each point 372 was lower than those for class I compounds.

Figure 5 shows the time when crystallinity reached 10%, t_{10} , 374 as a function of the reduced temperature, $T_{\rm g}/T$. In this figure,

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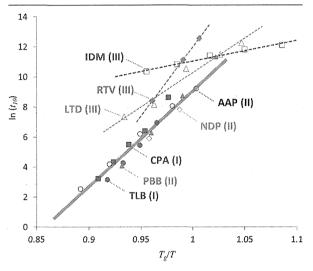


Figure 5. 10% crystallization time (initiation time, in the unit of min) as a function of T_g/T for all the model compounds. Symbols: TLB (\blacksquare), CPA (\blacksquare), AAP (\bigcirc), NDP (\bigcirc), LTD (\triangle), RTV (\spadesuit). Literature data for indomethacin (IDM, \square)²¹ and phenobarbital (PBB, \triangle)° is also presented. The fitting line ("general line") was drawn for TLB, CPA, AAP, NDP, and PBB, which showed temperature-dominated crystallization (i.e., thermodynamically controlled compounds) and can be expressed by $\ln(t_{10}) = 66.2(T_g/T) - 57.0$.

375 the literature data for indomethacin $(IDM)^{21}$ and phenobarbi-376 tal $(PBB)^9$ is also presented. Hereafter, t_{10} is referred to as the 377 initiation time. Note that the induction time, d, is a more 378 reasonable parameter for describing timing when crystallization 379 begins; however, the reliability of d obtained from Avrami 380 fitting is generally poor because of shape of logarithmic 381 function. The contrast, reliability of t_{10} value is much higher and 382 its validity can easily be judged from interpolation of the raw 383 data around 10% crystallinity. Even for cases where the 384 crystallization is very slow, t_{10} can be obtained without 385 performing experiments over a long period, while the entire 386 crystallization curve is required for obtaining d from the Avrami fitting. Thus, t_{10} is a practical parameter to evaluate the time 387 when crystallization begins.

The most important finding in Figure 5 is that the data for 389 classes I (TLB, CPA) and II (AAP, NDP, PBB) compounds fell 390 on the same line at least above $T_{\rm g}$. Thus, if crystallization of the $_{
m 391}$ compounds is governed by thermodynamics to some extent, 392 their initiation time can be described as a function of only $T_{\rm g}$. 393 The line passes through approximately $\ln(t_{10}) = 9$ at $T_g/T = 1$, 394 meaning that any class I and II compounds should start to 395 crystallize in 6 days at $T_{\rm g}$. Although this value has a deviation of $_{396}$ approximately one order, there is demonstrable universality in 397 the initiation time regardless of the compound species. The 398 slope of the universal line provides the ratio of activation energy 399 (E_a) for initiating crystallization to T_{σ} as ca. 550 J/(mol·K), and 400 from this value, E_a could be calculated as 217, 221, 243, and 245 401 kJ/mol, respectively, for CPA, TLB, AAP, and NDP. Thus, E_a 402 roughly correlates with the crystallization tendency (energetic 403 barrier for crystallization) during the cooling/heating cycle in 404 DSC, but the differences are not significant.

The initiation time for class III compounds (LTD, RTV, 406 IDM) was significantly longer than for class I and II 407 compounds, i.e., the thermodynamically controlled compounds. 408 The poor reproducibility in the crystallization behavior of these 409 compounds indicated that stochastic nucleation plays an 410 important role in determining the initiation time.

Relevance of Nucleation Mechanism to the Dominant 412 Factor for Crystallization. Figure 6 shows the Avrami 413 66

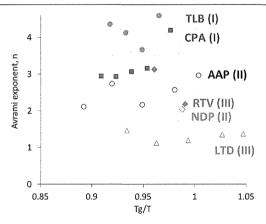
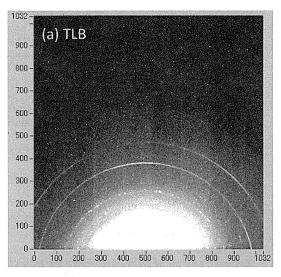


Figure 6. Avrami exponents as a function of $T_{\rm g}/T$ for all the model compounds, which were obtained by the fitting to the Avrami–Erofeev equation as shown in Figure 4. Symbols are the same as those for Figure 5

exponent obtained by fitting the Avrami–Erofeev equation. 414 The Avrami exponent, which depends on the nucleation 415 mechanism and dimensions of the crystal growth, generally 416 exhibited a large value for class I compounds, followed by class 417 II and III compounds. The value for TLB was constant at ca. 4, 418 which can only be understood by three-dimensional crystal 419 growth after homogeneous nucleation. It is most likely that 420 compounds of lower classes tend to nucleate homogeneously, 421 and with higher classes, the nucleation mechanism changes to 422 heterogeneous.

Synchrotron WAXD and DSC simultaneous measurements 424 were applied for observing crystallization of TLB and AAP. 425 Figure 7 shows two-dimensional WAXD after crystallization. 426 f7 TLB produced a diffraction ring pattern, indicating that small 427

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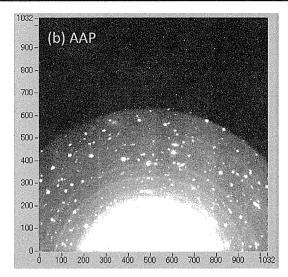


Figure 7. X-ray diffraction rings obtained for TLB and APP using synchrotron radiation source, which were crystallized during cooling at 5 °C/min and reheating at 5 °C/min, respectively.

428 nuclei were formed immediately, but the size of the grown 429 crystals was small. In contrast, a few nuclei should have been 430 produced for AAP, leading to the formation of large single 431 crystals because many diffraction spots were obtained in 432 WAXD. This result supports the assumption of the nucleation 433 mechanism based on the Avrami exponents. The thermody-434 namically controlled crystallization of class I compounds seems 435 to be closely related to their nucleation mechanism, which is 436 homogeneous nucleation. In contrast, the kinetic factor seems 437 to play a partial role in the crystallization behavior if the 438 nucleation is heterogeneous.

439 A similar observation on the relationship of the crystallization 440 rate, nucleation mechanism, and Avrami exponent was 441 previously made on the pharmaceutical ester oil, Imwitor 442 $742.^{23}$ It crystallized to the form α immediately upon cooling 443 below -20 °C, while a temperature-dependent slow crystal-444 lization to form β was observed above this temperature. The 445 microscopic observation indicated that the crystallization to the 446 forms α and β seemed be initiated by homogeneous and 447 heterogeneous nucleation, respectively. The Avrami exponent 448 was only available for the form β , and it also supported the 449 connection between slow crystallization and heterogeneous 450 nucleation. Furthermore, poor reproducibility in the induction 451 time for crystallization of the form β indicated that stochastic 452 nucleation played an important role in the case of the 453 heterogeneous nucleation.

Figure 8 shows the crystallization rate as a function of the lower class reduced temperature. The compounds of the lower class to the temperature as the first dependence of the crystallization rate itself, variation in the time influenced the calculation because it made the time required for crystallization apparently longer. If crystal-time required for crystallization apparently longer. If crystal-time required for crystallization analyzed individually, the crystallization rate should be smaller. Such analysis was the crystallization rate was not sensitive to temperature in the temperature range, where a long initiation time is required.

Quantitative Prediction of Storage Stability. If a trace 466 amount of crystals exists in the amorphous formulation, it 467 significantly enhances crystallization after dispersion to the

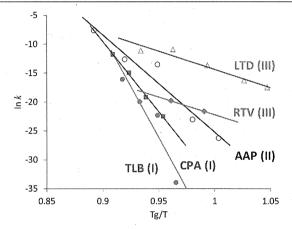


Figure 8. The crystallization rate as a function of reciprocal time. Symbols are the same as those for Figure 5

medium. The presence of 10% crystal would be sufficient to 468 impair the advantage of amorphous dosage forms. Thus, the 469 most important parameter to be predicted in the developmental 470 study is the initiation time despite a wide variation in the 471 crystallization rate after nucleation. Figure 9 shows the 472 f9 initiation time of the crystallization as a function of $T_{\rm g}$ for 473 compounds in which crystallization is basically governed by 474 thermodynamics (classes I and II). If a three-year stability is 475 desired, Tg must be higher than 48 or 26 °C for storage at 25 or 476 5 °C, respectively. The differences between the critical T_{σ} and 477 storage temperature are 23 and 21 °C, respectively. Class III 478 compounds should be more stable; however, a sufficient 479 stability margin must be considered because of the poor 480 reproducibility in the crystallization behavior. The initiation 481 time for thermodynamically controlled compounds may be 482 regarded as the worst case for class III compounds. In 483 conclusion, the "shortest" initiation time for any compound can 484 be generalized by the universal line shown in Figure 5, which 485 provides more optimistic criteria than the $T_{\rm g}$ -50 °C rule.² It 486 should be noted that the "general line" in Figure 5 was basically 487

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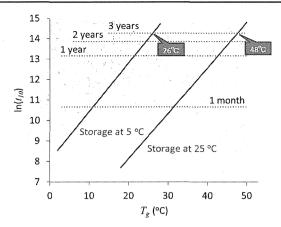


Figure 9. Initiation time of the thermodynamically controlled crystallization as a function of the glass transition temperature. The general line in Figure 5 was used for the calculation by assuming storage at 5 or 25 °C.

488 drawn using the data above $T_{\rm g}$. Validity of its extrapolation to 489 the lower temperature requires further investigation.

The formulation stability should be much better than that of 491 the amorphous drug. In this paper, only the stability of the drug 492 molecule is discussed which can be regarded as the worst case 493 for formulation stability. It is also expected to be predicted from 494 the mixture T_g ; however, much care is required for miscibility in 495 multicomponent systems. Although molecular-level mixing 496 between drug and excipient molecules is expected for 497 amorphous formulations, current analysis techniques only 498 allow for investigation of miscibility on larger scales. For 499 example, DSC is usually investigating miscibility on a 10-100 500 nm scale.²⁴ Although solid-state nuclear magnetic resonance 501 can evaluate smaller scale miscibility, the lower limit is a few 502 nanometers.²⁴ Moreover, miscibility can change during storage 503 and even during measurements. 25 If molecular clusters of drug 504 molecules, of which the size may be below nano-order, exist in 505 the formulation, the formulation stability may almost be equal 506 to drug stability, which can be predicted as presented in this 507 study.

The surface area of the melts was minimized and their 509 contact with moisture was shielded in this study. If the 510 formulation is prepared by hot-melt extrusion without applying 511 subsequent milling, a similar level of stability may be achieved. 512 However, powder formulations will have a lower stability than 513 those of the melts because crystallization is frequently initiated 514 at the surface. 26-28 Further studies that consider the effect of 515 surface area and contact with moisture must be performed to 516 establish a more general idea for predicting the physical stability 517 of practical amorphous formulations.

518 CONCLUSIONS

519 Crystallization behaviors of pharmaceutical glasses which have 520 wide variation in crystallization tendency during cooling from 521 the melt have been investigated. The classification system 522 proposed by Taylor et al. was employed for evaluating relative 523 contributions of thermodynamic and kinetic factors in the 524 crystallization process. The class I compounds, for which the 525 thermodynamic factor (temperature) plays a dominant role, 526 exhibited high reproducibility in the crystallization rate, 527 probably due to their homogeneous nucleation. Crystallization 528 of the class II compounds was also essentially governed by thermodynamics; however, the nucleation might be heteroge- 529 neous, which led to lower reproducibility in crystallization 530 behavior than that for the class I compounds. The initiation 531 time for crystallization of class I and II compounds had 532 universal activation energy, ca. 210-250 kJ/mol, and thus could 533 be generalized as a function of only $T_{\rm o}/T$. As for the class III 534 compounds, the crystallization appeared to be initiated by 535 stochastic nucleation. Better stability is expected for the class III 536 compounds, although reproducibility in crystallization was 537 lower than for the class I and II compounds. This analysis 538 should make the physical stability of pharmaceutical glasses 539 predictable.

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Research Article

Simultaneous Determination of Polyethylene Glycol-Conjugated Liposome Components by Using Reversed-Phase High-Performance Liquid Chromatography with UV and Evaporative Light Scattering Detection

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Abstract. Liposomes incorporating polyethylene glycol (PEG)-conjugated lipids (PEGylated liposomes) have attracted attention as drug delivery carriers because they show good in vivo stability. The lipid component of PEGylated liposomal formulations needs to be quantified for quality control. In this study, a simple reversed-phase high-performance liquid chromatography (HPLC) method with an evaporative light-scattering detector (ELSD) was established for simultaneous determination of hydrogenated soy phosphatidylcholine, cholesterol, PEG-conjugated lipid, and hydrolysis products of phospholipid in PEGylated liposomal formulations. These lipids were separated using a C18 column with a gradient mobile phase consisting of ammonium acetate buffer and ammonium acetate in methanol at a flow rate of 1.0 ml/min. This method provided sufficient repeatability, linearity, and recovery rate for all lipids. However, the linearity and recovery rates of cholesterol achieved using a ultraviolet (UV) detector were better than those achieved using an ELSD. This validated method can be applied to assess the composition change during the preparation process of liposomes and to quantify lipid components and hydrolysis products contained in a commercially available liposomal formulation DOXIL®. Taken together, this reversed-phase HPLC-UV/ELSD method may be useful for the rapid or routine analysis of liposomal lipid components in process development and quality control.

KEYWORDS: component analysis; evaporative light scattering; liposome; reversed-phase HPLC.

INTRODUCTION

Liposomes, which are closed vesicles consisting of a lipid bilayer, have been studied as drug delivery carriers, and have been applied in clinical treatments. It is well known that liposomes incorporating polyethylene glycol (PEG)-conjugated lipid (PEGylated liposomes) can escape uptake by the reticuloendothelial system (RES) and circulate in the blood stream for a prolonged period of time (1,2). Moreover, PEGylated liposomal doxorubicin—DOXIL®—has been marketed and is available commercially. Ambisome®, which contains amphotericin B in the lipid bilayer, demonstrates properties that tend to be uptaken by RES because of anionic lipids in the bilayer and exhibits anti-fungal effects within the RES (3). In gene delivery, cationic liposomes are widely used and numerous attempts have been made to increase the gene transfection efficiency by using ligand-modifying and functional lipids (4). Thus, the "liposome" does not exist, and the lipid

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component of liposomes is dependent on the encapsulated drug or the objective product performance. Therefore, the lipid and polymeric modifier composition is one of the important physicochemical properties to ensure the quality/safety/efficacy of liposomal products.

Hydrolysis is the primary chemical degradation process of phospholipids. The hydrolysis of ester functionalities is unavoidable in the presence of water, which results in the production of lysophospholipids and free fatty acids. Lysophospholipids may also be further degraded into glycerophosphorylcholine and free fatty acids. It has been reported that increased concentrations of degradation products in liposomal formulations enhance permeability and cause destabilization of the lipid bilayer (5), which significantly affects particle size and can change the structure of the lipid assembly from lamellar to micellar (6). Thus, lipid hydrolysis is considered a critical parameter for the chemical stability of liposomal products. A considerable amount of research has been conducted on the factors that affect the hydrolysis rate, including pH and ionic strength of the storage solution (7-9). Because of these factors, the "assay of lipid components" and "degradation products related to the lipids" are recommended for pharmaceutical specifications in the draft guidance presented by the US FDA for liposomal products (10). This guidance also recommends the development of a stability test which would help evaluate the chemical stability of lipids in liposomal formulations as well as the stability of the

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encapsulated drug, by measuring degradation products such as lysophospholipids and free fatty acids. Thus, appropriate methods for the quantification of lysophospholipids and free fatty acids as well as the liposomal components are required to ensure the efficacy and safety of liposomal products.

High-performance liquid chromatography (HPLC) is widely used to separate and analyze lipids of various origins into lipid classes or molecular species. While unsaturated lipids may be analyzed by ultraviolet (UV) detection, saturated lipids, which are commonly used in liposomal formulations, have no specific absorbance in the UV region, and conventional UV detection cannot be used unless derivatized. Thus, the refractive index detector (RID), evaporative light-scattering detector (ELSD), charged aerosol detector (CAD), and MS were applied for the simultaneous HPLC analysis of lipids (8,11-13). Since ELSDs are higher sensitivity than that exhibited by RIDs, compatible with gradient elution, more easily available than CAD, and simpler to maintain than LC-MS, they are widely used for lipid analyses. Several HPLC-ELSD methods for the analysis of lipids or the hydrolysis products of phospholipids have been previously reported; however, the normal-phase separation was often used, which resulted in the large consumption of chloroform (14-17). While the reversed-phase separation method for the analysis of lipids in cationic liposomes have been reported (18), the reversed-phase separation methods for the simultaneous analysis of PEG-conjugated lipid and the hydrolysis products in PEGylated liposomes have not been well studied. Thus, in this study, we attempted to develop a reversed-phase HPLC-ELSD system that could simultaneously analyze the lipid components and hydrolysis products in PEGylated liposomes.

MATERIALS AND METHODS

Materials and Buffer Solutions

Hydrogenated soy phosphatidylcholine (HSPC; C16:0, 11.4% and C18:0, 88.6%) and N-(carbonyl-methoxy polyethyleneglycol 2000)-1,2-distearoyl-sn-glycero-3-phosphoethanolamine (DSPE-PEG), 1-palmitoyl-2-lyso-sn-glycero-3-phosphocholine (P-LysoPC), and 1-stearoyl-2-lyso-sn-glycero-3-phosphocholine (S-LysoPC) were purchased from Nippon Oil and Fat (Tokyo, Japan). Analytical-grade cholesterol (Chol), palmitic acid (PA), stearic acid (SA), HPLC-grade methanol, and ammonium acetate were purchased from Wako Pure Chemical (Osaka, Japan). Trifluoroacetic acid (TFA) was from Sigma-Aldrich Co (MO). Four lots (#011AFL, 012AGD, 029BJD, and 032BKA) of DOXIL® (JANSSEN PHARMA-CEUTICAL K.K, Tokyo, Japan) were purchased from a general sales agency for drugs, and the approximate elapsed time of each lot after manufacture was 68, 65, 29, and 26 months, respectively.

Standard stock solutions of PA, SA, P-LysoPC, S-LysoPC, HSPC, Chol, and DSPE-PEG were individually prepared by dissolving 3.0 mg of each lipid in 10 ml of methanol and stored at 4°C. The calibration standards were then prepared by diluting the standard stock solutions with methanol.

Instrumentation and Chromatographic Conditions

The apparatus used for the HPLC system consisted of two constant pumps (LC-10ADvp, Shimadzu, Kyoto, Japan),

a degasser (DGU-14A, Shimadzu), an automated pretreatment system, an autoinjector (SIL-10ADvp, Shimadzu), a column oven (CTO-10ACvp, Shimadzu), a UV detector (SPC-20AV, Shimadzu), an ELSD (ELSD-LTII, Shimadzu), and a system controller (SCL-10Asp, Shimadzu). A nitrogen generator (SLP-221ED, ANEST IWATA, Yokohama, Japan) was used as the source for the nitrogen gas. Data analysis was performed with the LC Solution program (Shimadzu). The separation was performed at 45°C on a YMC-Triart C18 column (150×4.6 mm i.d., 5 µm) from the YMC Co. (Kyoto, Japan). The ELSD conditions were as follows: the drift tube temperature was set at 45°C, the nitrogen gas-pressure was set at 350 kPa, and the gain was set to 6. The flow rate was 1.0 ml/min for the mobile phases (mobile phase A, 4 mM ammonium acetate buffer (pH 4.0) and mobile phase B, 4 mM ammonium acetate in methanol). The binary linear gradient began from a mixture of 20% A and 80% B and ended at 100% B in 10 min. After the 10-min plateau at 100% B, the mobile phase composition changed back to its initial composition in 5 min. The liposome samples were directly diluted with methanol to the lipid concentration within the calibration range. DOXIL® was diluted 10- or 20-fold, and the liposomes under the preparation were 10-fold diluted. The sample injection volume was 20 µl.

Liposomal Preparation

The lipid composition of PEGylated liposome referred to DOXIL®. The liposome, which consisted of HSPC/Chol/ DSPE-PEG, was prepared using a modified ethanol injection method (19). Briefly, 47.9 mg of HSPC, 15.95 mg of Chol, and 15.95 mg of DSPE-PEG were dissolved in approximately 10 ml of ethanol. The ethanol was then removed using a rotary evaporator, which left behind approximately 1 ml of ethanol solution. Next, 8 ml of 10% sucrose (pH 6.5) was added to the ethanol solution. Liposomes formed spontaneously after further evaporation of the residual ethanol, and were extruded through a series of polycarbonate filters (Nucleopore, CA) with pore sizes ranging from 0.4 to 0.1 µm. Following the extrusion, the liposome solution was placed in membrane tubing with a molecular weight cut-off of 50 kDa (Flat-A-Lyzer G2, Spectrum Laboratories, Inc., CA) and was dialyzed against fresh 10% sucrose solution to remove the free lipids or micelles.

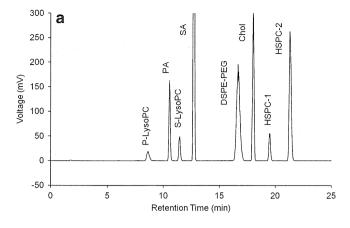
Incubation of Liposome

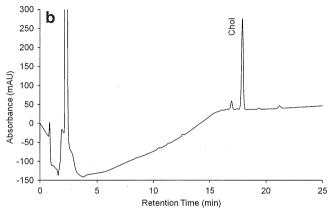
Each 500 μ l of liposome in glass tubes were incubated at 37°C or 57°C in a water bath without agitation, or at 4°C in a refrigerator for three days. After incubation, liposomes were diluted 10-fold with methanol, and 20 μ l of aliquots were injected to HPLC system.

RESULTS AND DISCUSSION

Optimization of the Separation Conditions

The method for the quantification of lipids in a laboratory preparation of liposomes as well as liposomal formulation development and quality control should be simple, rapid, and safe. Thus, we aimed to develop an HPLC-ELSD system that would quickly and simultaneously separate all of the





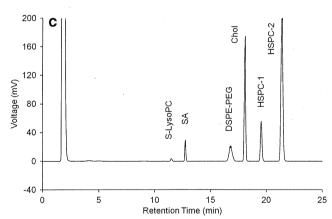
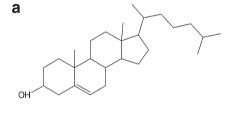


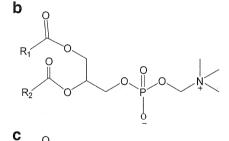
Fig. 1. Comparison of the chromatograms detected by ELSD (a) and UV (b). A standard mixture (20 μ l) containing 150 μ g/ml (each) of P-LysoPC, S-LysoPC, PA, and SA; 300 μ g/ml of Chol; and 750 μ g/ml each of HSPC and DSPE-PEG was injected. The chromatogram of DOXIL® detected by ELSD (c). DOXIL® was diluted 10-fold with methanol, and 20- μ l aliquots of the diluted solution were injected

lipids in the PEGylated liposomal formulations, which are not only liposomal lipids, but also the hydrolyzed products (lysophospholipids and free fatty acids). It has been reported that the hydrolysis of phosphatidylcholine predominantly produces 1-acyl-2-lyso-phosphatidylcholine with free fatty acids (8). Thus, 1-acyl-2-lysoforms were analyzed. Consistent with previous reports describing reversed-phase HPLC methods for lipids (18), the HPLC separation was optimized using a

C18 column with TFA or ammonium acetate in methanol. However, the mobile phase with TFA did not provide a reproducible retention time for DSPE-PEG, and thus the mobile phase with ammonium acetate was selected. Using an isocratic elution with methanol-ammonium acetate buffer, a stable separation of lipid components, lysoforms, and fatty acids was obtained after optimization of the volume ratio, concentration, and pH of the ammonium acetate buffer (Figs. 1, 2, 3, and 4 in the Electronic Supplementary Materials). The HSPC, which consists of fatty acids, C16 and C18, showed two peaks, HSPC-1 and HSPC-2. Since PEG has a distribution of molecular weight, the peak shape of DSPE-PEG was broad. While there were no effects on the concentration of ammonium acetate (25-400 mM) on the Chol and HSPC, the higher concentration of ammonium acetate was associated with the faster retention time of DSPE-PEG. Although the details remain unclear, a large amount of ammonium ions may ionically interact with the anionic portion of the DSPE-PEG and increase its polarity.

The separation of the lipid components and hydrolysis products was possible using an isocratic mobile phase with methanol–200 mM ammonium acetate buffer (pH 4.0) (98:2, ν/ν). To clearly separate the lysoforms and fatty acids from the highly polar materials in the liposomal formulations, such as the active ingredient and sucrose, gradient elution was optimized. To maintain a steady level of ammonium acetate, 4 mM





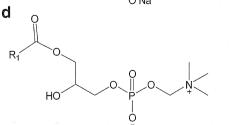


Fig. 2. Structure of a cholesterol, b HSPC, c DSPE-PEG, and d S-LysoPC)

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Table I. Variability of Retention Times and Peak Areas of Standard Lipids (n=6), Limits of Detection (LOD), and Limits of Quantification (LOQ)

		Within-day	ay Between-day				
Lipid	Concentration (µg/ml)	Retention time (min, RSD)	Average area (mVs, RSD)	Retention time (min, RSD)	Average area (mVs, RSD)	LOD (µg/ml)	LOQ (µg/ml)
S-LysoPC	22.5	10.90 (0.33)	69.40 (3.62)	10.90 (0.13)	71.35 (4.20)	3.65	7.95
SA	12	12.33 (0.20)	316.22 (2.86)	12.33 (0.17)	334.65 (4.58)	1.31	2.36
DSPE-PEG	.75	16.28 (0.16)	282.59 (1.68)	16.28 (0.08)	283.79 (1.55)	5.92	15.06
Chol	75	17.47 (0.06)	1,209.61 (2.81)	17.47 (0.05)	1,220.09 (2.64)	2.48	4.77
HSPC-1	240	18.75 (0.06)	267.60 (2.62)	18.76 (0.12)	257.80 (3.56)	12.42	34.35
HSPC-2	240	20.33 (0.07)	1,675.54 (2.41)	20.34 (0.13)	1,668.74 (2.95)	5.47	14.28

RSD relative standard deviation

ammonium acetate in methanol and 4 mM ammonium acetate buffer were used. The standard mixture which was diluted by methanol to obtain the target concentration was injected into the HPLC equipment, and sequentially monitored using a UV detector (205 nm) and the ELSD. A typical chromatogram is shown in Fig. 1a. Lipids were eluted in the order P-LysoPC, PA, S-LysoPC, SA, DSPE-PEG, Chol, HSPC-1, and HSPC-2 (Fig. 1a). Only the peak of the Chol was detectable using the UV detector; however, the other peaks could not be sufficiently obtained because of a lack of a C-C double bond (Fig. 1b). In contrast, higher and sharper peaks for all of the lipids were obtained using the ELSD (Fig. 1a). Next, to confirm the separation of the lipids from the additives in liposomal products, DOXIL® was diluted with methanol and injected into the HPLC equipment. A typical chromatogram is shown in Fig. 1c. Following the elution of highly polar materials such as doxorubicin and sucrose, the peaks of the hydrolysis products (S-LysoPC and SA) and lipid components in DOXIL® were obtained. Figure 2 shows the chemical structure of Chol and phospholipids detected in the sample of DOXIL®. Thus, the optimized analytical condition may be considered to exhibit sufficient sensitivity and separation for the quantification of lipid components and hydrolysis products in the liposomal products.

Method Validation

The developed HPLC-ELSD method for the analysis of lipids (S-LysoPC, SA, DSPE-PEG, Chol, HSPC-1, and HSPC-2) was validated with respect to repeatability, linearity, limits of detection (LOD) and quantification (LOQ), and accuracy (recovery rate). The within-day/between-day variability of the retention time and peak area of each lipid was evaluated (Table I). The between-day variability was determined on three different days by two different analysts. The relative standard deviation (RSD) values of the retention times were less than 0.33% for all lipids. For the peak areas, the RSD values using ELSD were higher. The LOD and LOQ for each lipid were evaluated (Table I). The LOD and LOQ values were calculated as three times the variation in the measured response (signal/noise ratio= 3) and ten times the variation (signal/noise=10), respectively. The values of the Chol and HSPC were the same number of digits as previously reported, which may be sufficient to determine the concentration of each lipid in the liposomal products.

Next, the linearity was tested for all lipids. Consistent with previous reports (20), the ELSD response was exponential rather than linear. The relationship between the peak area (A) and the concentration of each lipid (m) can be described as follows:

Table II. Standard Curves of Lipids in Methanol

Lipid		Regression equation	r^2
S-LysoPC (9.375–300 μg/ml)	Day 1	$y=98.049x^{1.6437}$	0.9985
, , , , , ,	Day 2	$y=130.83x^{1.6063}$	0.9989
	Day 3	$y=124.16x^{1.6416}$	0.9988
SA (4.688–150 μg/ml)	Day 1	$y=493.39x^{1.9887}$	0.9992
, ,	Day 2	$y = 750.9x^{1.8791}$	0.9987
	Day 3	$y=525.74x^{2.027}$	0.9989
DSPE-PEG (18.75–600 μg/ml)	Day 1	$y = 64.29x^{1.6745}$	0.9999
, , ,	Day 2	$y = 64.848x^{1.6856}$	0.9999
	Day 3	$y=89.084x^{1.6294}$	0.9989
Chol (37.5–600 µg/ml)	Day 1	$y=5,759.3x^{1.0923}$	0.9957
	Day 2	$y=4,940.5x^{1.1139}$	0.9916
	Day 3	$y=4,722.9x^{1.1246}$	0.9950
HSPC-1 (46.875–1,500 μg/ml)	Day 1	$y=7.0282x^{1.7086}$	0.9995
, , , ,	Day 2	$y=9.382x^{1.6658}$	0.9986
	Day 3	$y=9.2723x^{1.6605}$	0.9988
HSPC-2 (46.875–1,500 μg/ml)	Day 1	$y=31.233x^{1.7563}$	0.9980
	Day 2	$v=28.229x^{1.7698}$	0.9977
	Day 3	$y=21.056x^{1.8172}$	0.9973

Table III. The Recovery of the Lipid at Three Levels of Concentration: Accuracy of the HPLC-ELSD Method (*n*=3)

Lipid	Spiked concentration (µg/ml)	Recovered concentration (µg/ml)	Recovery (%)
S-LysoPC	15	15.02	100.10
	30	30.01	100.05
	60	58.57	97.62
SA	7.5	7.21	103.80
	15	14.76	98.42
	30	29.71	99.03
DSPE-PEG	75	74.77	99.69
	150	150.42	100.28
	300	302.67	100.89
Chol	75	85.38	113.83
	150	141.01	94.01
	300	285.06	95.02
HSPC-1	240	238.36	99.32
	480	468.95	98.59
	960	944.01	98.33
HSPC-2	240	238.99	99.58
	480	501.58	103.37
	960	964.63	100.48

A=am^b, where a and b are constants that are dependent on a variety of experimental conditions. A linear relationship was observed between the log (peak area) versus log (lipid concentration) for all lipids on three different days, where the correlation coefficients of S-LysoPC, SA, DSPE-PEG, HSPC-1, and HSPC-2 were greater than 0.997 (Table II). However, the correlation coefficient of Chol tended to be lower, from 0.9916 to 0.9957.

Recovery was assessed at low, medium, and high concentration levels of lipids. A stock standard solution for each lipid was diluted with methanol/10% sucrose (90/10, v/v) to obtain the theoretical concentration indicated in Table III, and three diluted solutions were individually injected. The average concentration was measured using the standard calibration curve of each lipid, and the average recovery rate was calculated based on the measured concentration against the theoretical concentration of each lipids. The recovery rates, except those for Chol, were 97.62-103.80%, indicating sufficient accuracy. The recovery rate of Chol was 94.01-113.83%, which did not suggest good accuracy. Because UV could sufficiently detect Chol as shown in Fig. 1, Chol was analyzed using the UV detector, which was placed in series with the ELSD, and the recovery rate for Chol was calculated (Table IV). The correlation coefficient for the calibration curve of Chol (e.g. y=7,774.4x+46,171) was 0.9999, and the recovery rate was 100.73-101.3%, indicating sufficient

Table IV. The Recovery Rate of Chol at Three Levels of Concentration: Accuracy of the HPLC-UV Method (*n*=3)

Lipid	Spiked concentration (µg/ml)	Recovered concentration (µg/ml)	RSD (%)	Recovery (%)
Chol	75	75.55	0.10	100.73
	150	151.94	0.10	101.30
	300	303.56	0.03	101.19

Table V. Effect of Processing Stage on Liposome Component (n=3)

	Calculated lipid molar ratio (mean±SD; %					
Processing stage	Chol ^a	HSPC^b	DSPE-PEG			
Dissolved in ethanol Evapolation Particle size reduction Dialysis	40.48±0.32 40.72±0.04 40.73±0.45 42.47±0.74	54.13 ± 0.32 53.99 ± 0.11 53.99 ± 0.54 53.02 ± 0.55	5.39 ± 0.13 5.29 ± 0.10 5.29 ± 0.12 4.51 ± 0.33			

^a Chol was detected by a UV detector

linearity and accuracy. These results indicated that the HPLC-ELSD method is applicable to the measurement of lipid components and hydrolysis products in liposomal formulation, while in the case of Chol, UV detection will be better using the same separation system. The low linearity of Chol, not additives in samples, can be considered a cause for the inadequate recovery rate because even the sample containing only Chol and methanol showed low recovery rate (data not shown). After an investigation, it was found that ammonium acetate in mobile phase affects the detection process of ELSD (droplet size/density/distribution by nebulization, and size/distribution of evaporated particles), and can cause a lower correlation coefficient between concentration and scattering intensity.

Application of the Method

A validated HPLC-UV/ELSD method was first used for the quantitative analysis of liposomes prepared in our laboratory. To quantify the HSPC, the main HSPC-1 peak was evaluated based on the linearity of both peaks. Adequate quantification of the prepared liposomes is critical to maintain the attributes (such as encapsulation efficiency and lipid composition rate) of the liposomal formulation. Moreover, the evaluation of changes in lipid composition will be needed to properly design the preparation (manufacturing) process. Changes in the lipid composition rate were assessed in the liposome preparation process (Table V). Compared with the lipid composition when lipids were dissolved in ethanol, there were no significant changes after the evaporation and particle size reduction. However, after the dialysis for external solution exchange, the percentages of HSPC and DSPE-PEG slightly decreased, whereas the percentage of Chol was slightly increased. The total lipid amount decreased by 5-10% following dialysis (data not shown). Thus, changes in the lipid component may be caused by the removal of HSPC and DSPE-PEG, which is not incorporated into the liposome, from the dispersing solution by dialysis.

Next, DOXIL® was quantified. Four product lots that were stored for a long period of time were compared. Two lots were stored for over 65 months and two lots were stored for 26–29 months (Table VI). Compared with the lipid composition described in the package insert of DOXIL®, the ratio of Chol was slightly higher, and the ratios of HSPC and DSPE-PEG were slightly lower. These slight differences may have been caused by the liposomal preparation process because the lipid composition described in the package insert was the quantity of

^b The value of HSPC was calculated from the peak of HSPC-1