## 分子心血管病

別刷

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# ナノサーフェーステクノロジーによる新規生体適合性表面処理 Toyobo-NCVC コーティングの開発と補助人工心臓および膜型人工肺への応用

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#### SUMMARY

われわれは、従来から開発をおこなってきたナノサーフェーステクノロジーを応用し、コーティング剤の分子構造をナノ単位で制御し、血液適合性への最適化を図ることにより、血液界面における長期間の血液凝固防止作用の維持を可能とした、新しいコンセプトの Toyobo-NCVC コーティングを開発しえた。本技術は、既存の人工心臓(国立循環器病センター型空気駆動式補助人工心臓、東洋紡積社製)および膜型人工肺(Platinum Cube NCVC シリーズ、大日本インキ社製)に採用され、その長期的な抗血栓性を飛躍的に向上させ、その長期使用における安全性の維持に大きく貢献すると考えられた。

#### POINTS

- ■Toyobo-NCVC コーティングは,すぐれた血液適合性と長期耐久性を実現する新規表面処理法である.
- ■Toyobo-NCVC コーティングは、人工心臓や膜型人工肺の安全性の向上に寄与する新技術である。
- ■次世代型人工臓器開発には、より高性能で安定した生体適合性をもつ表面処理技術の開発が必要である。

#### KEY WORDS

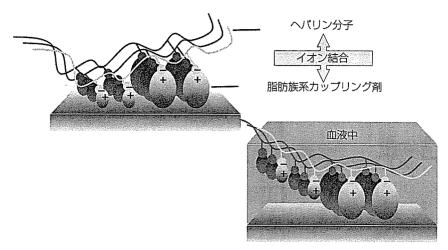
ナノサーフェーステクノロジー,生体適合性表面処理技術,人工臓器,抗血栓性素材

#### 園 はじめに

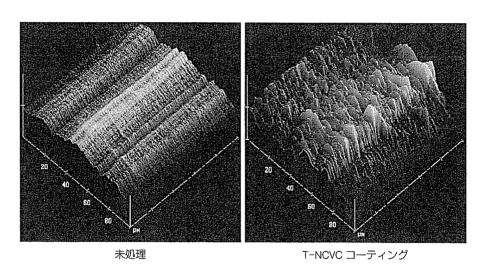
近年,人工心臓および人工肺などの循環器系人工臓器では,血液と接する器材の表面に血栓形成を抑制する種々の血液適合化処理をおこなうことが一般的になっている. 従来の研究では,器材表面での血栓形成を防止するための理論的手法として,器材表面の均一化(平滑化),器材表面への血漿蛋白質吸着の防止(材料表面の性質の制御による抗血栓性の賦与),器材表面に血液凝固防止剤(ヘパリンなど)を固定化する方法(抗血栓物質の利用)

など多くの研究がなされている<sup>1)</sup>. しかし, いずれの方法 においても, その効果を長期的に維持することは困難で あり, いまだに十分な技術の確立がなされてはいない.

われわれは、かかる問題に対し従来から研究をおこなっているコーティング材の分子構造制御法(ナノサーフェーステクノロジー)により、血液と接する材料表面の生体適合性能を最適化し、長期間の血液凝固防止作用の維持を可能とした Toyobo-NCVC(T-NCVC)コーティングを開発しえた<sup>2)</sup>. 本技術は、ナノサーフェーステクノロジーにより分子単位で制御された長鎖ジアルキル



図**●** T-NCVC コーティングの概念図 (西中知博ら, 2002<sup>4)</sup>より改変引用)



図② T-NCVC コーティングのナノ表面構造 T-NCVC コーティングの超微細構造は、未処理のポリスチレン平面と比較し、顆 粒状の表面を有する。

基を有する脂肪族系カップリング剤とヘパリンの複合体からなる新たな血液適合化処理技術であり、従来技術では短期の抗血栓効果しか望めなかったイオンコーティング法の欠点を克服し、長期の抗血栓効果を保持することを可能とした。また、類似するほかのヘパリンコーティング法と比較しても、処理工程が簡便で、比較的安価で提供できることを特徴としている。T-NCVCコーティングは、すでに製品化されている人工心臓(国立循環器病センター型空気圧駆動式補助人工心臓、東洋紡績社製)および膜型人工肺(Platinum Cube NCVCシリーズ、大日本インキ社製)に採用され、その長期的な抗血栓性を

飛躍的に向上させることにより、その長期使用における 安全性の維持に大きく貢献している<sup>3)4)</sup>.

### I T-NCVC コーティングのナノ表面性状と抗血栓性機序

われわれが東洋紡績社と共同開発をおこなった T-NCVC コーティングは、複数の長鎖ジアルキル基を有する脂肪族系カップリング剤とヘパリンのイオン結合型複合体で、ナノサーフェーステクノロジー技術を応用し、その分子構造にナノ単位のアレンジを加え、血液界面に

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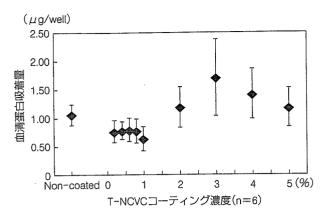


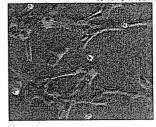
図3 T-NCVC コーティング各濃度における血漿蛋白吸 着の変化

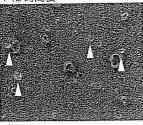
高濃度の T-NCVC コーティング処理後には、無処 理ポリスチレン表面にくらべ、血漿中の蛋白が吸着 しやすい性質になっている.

対するコーティング材の最適化をおこなうことにより, 血液に対する適合性を向上させた新規表面処理技術であ る(図①)、T-NCVC コーティングは、その表面超微細 構造が 200~500 nm の凹凸をくり返す顆粒状構造で(図 ②)、器材への血漿蛋白の吸着性についても、コーティン グ材表面に多量の蛋白を吸着させる傾向を有し(図❸), 従来法とは異なった独自のコンセプトで設計されてい る. さらに T-NCVC コーティングは, 非常にすぐれた細 胞接着阻害能を特徴とし、本コーティングに対する培養 線維芽細胞の接着実験では、静置培養24時間後において も、コーティングを施した培養皿底面への線維芽細胞の 接着や仮足の伸展などは認められず、細胞は球形のまま 培養維持が可能であることが示された(図Φ). また, T-NCVC コーティングの細胞接着阻害能は、培養液中に フィブロネクチンないしビトロネクチンを添加し、細胞 の接着作用を促進させた状態においても、その阻害効果 が低下することはなく、非常に安定的であることが認め られている.

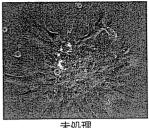
一般的に、ヘパリン化材料を含む人工材料表面は、固 相化されたヘパリンの徐放による血液凝固阻止作用を主 な抗血栓性機序として設計されている<sup>5)</sup>. したがって, イ オンコーティング法によるへパリン化材料については、 使用に伴う固相化へパリン量の減少と血漿蛋白の吸着に より抗血栓性能が低下していくため、長期的な効果を望 むことは困難であった<sup>6)</sup>. しかしながら, T-NCVC コー

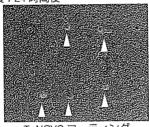
線維芽細胞培養; 12 時間後





線維芽細胞培養;24時間後



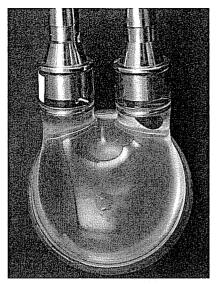


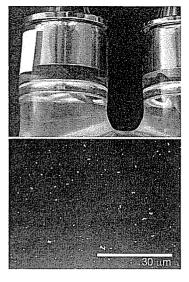
未机理

T-NCVC =

図4 T-NCVC コーティングの細胞接着阻害効果 T-NCVC コーティング上では、線維芽細胞培養24 時間経過後においても,培養細胞は底面に付着せず, 仮足の形成もおこなわれない (矢頭).

ティングでは、器材表面からのヘパリンの徐放過程を制 御することにより長期使用時における器材表面のへパリ ン残存量を増加させるとともに、器材表面の脂質成分上 に高濃度の硫酸多糖類層を形成することで生体細胞膜に 近い表面性状を模倣し,コーティング表面に吸着した細 胞接着性蛋白の存在に左右されない安定した細胞接着阻 止能を付与しえた、その結果、従来法の欠点を克服し、 実際にすぐれた抗血栓性を長期に維持することが可能と なった、さらに T-NCVC コーティング処理過程は、多種 の金属および高分子医療材料に塗布するだけの簡便な手 法で、その材料の抗血栓性を向上させることが可能と考 えられる。したがって、本新規血液適合化表面処理技術 は、その使用に際して、抗凝血療法の併用を最小限度に 止めることが可能であり、また、器材からのヘパリンな ど血液凝固阻害物質の徐放がきわめて微量なため、術後 の出血性合併症の発生を抑制することが期待され、これ からの循環器系人工臓器の長期使用時における安全性の 寄与に貢献できる新技術として注目されている.





図● T-NCVC コーティング国立循環器病センター型空気圧駆動式補助人工心臓 91 日間の長期動物実験後においても,人工心臓内に明らかな血栓形成は認められない。 (西中知博ら,2005°)より改変引用)

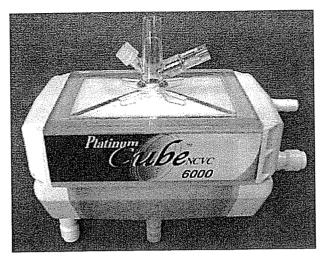
#### ■ II. T-NCVC コーティン グ国 立循 環器病センター型空気圧駆動式 補助人工心臓

人工心臓は、重症心不全患者の移植までのブリッジ使用(Bridge to Transplantation)や再び心機能を回復するまでの機能補助(Bridge to Recovery)を目的とする短、中期的な治療手段の1つとして改めて認識されている。しかし一方では、心機能の回復を見込めない症例に対する恒久的な使用を目的とした Destination Therapyに対する有用なツールとしての期待も高まっている。その結果、重症心不全患者に対する人工心臓の有用性の再認識とともに患者の QOL(quality of life)を考慮した、より安全に長期間使用できる人工心臓システムの開発が急務となっている。

このような現状において、わが国で主に使用されている国立循環器病センター型空気圧駆動式補助人工心臓(Toyobo-NCVC VAS)を長期的かつ安全に使用するための改良は、非常に意義深いものである。そのための重要な課題の1つは、人工心臓の抗血栓性を向上させ、使用患者の血栓塞栓症の発生率を低下させることであり、、欧米諸国ではすでに補助人工心臓の血液ポンプ表面にへ

パリン化処理を施し、その抗血栓性を向上させる試みが なされ、良好な結果が得られつつある.

そこで、われわれはこの Toyobo-NCVC VAS に対 し、ナノサーフェーステクノロジーから生み出された T-NCVC コーティングを施すことにより、Toyobo-NCVC VAS の抗血栓性を飛躍的に向上させ、長期使用 への安全性を向上させることを目標に開発をおこなって きた、国立循環器病センター研究所でおこなわれた前臨 床的動物実験では、この T-NCVC コーティングを施し た改良型 Toyobo-NCVC VAS を,成ヤギに左心バイパ ス方式で装着し、最長154日間連続的に駆動することに より、その長期的な抗血栓性について検討をおこなった. 本動物実験に際しては、ワーファリン投与など抗凝血療 法は一切おこなわず、血圧モニター用ライン維持を目的 としたヘパリンのきわめて微量な投与をおこなうのみで あったが, 実験終了後の血液ポンプ内の血栓形成状態は, 弁輪周囲のわずかな部位に認められたのみであり、ポン プの血液室内に形成される血栓は顕著に抑制されていた (図**⑤**). 本研究により, T-NCVC コーティングは, 血液 ポンプの耐久性に関連する物理的および化学的特性に変 化を与えることなく、従来と同様の耐久性を維持しなが ら、ポンプの抗血栓性能を顕著に向上させることが示さ



図**6** T-NCVC コーティング膜型人工肺 Platinum Cube NCVC 6000

れた。また、T-NCVCコーティング Toyobo-NCVC VAS は、2005 (平成17)年に厚生労働省より医療機器として承認を受け、今後臨床使用が開始される見込みであり、補助時人工心臓装着患者の臨床成績の向上に貢献できることが期待されている。

#### ■ III. T-NCVC コーティング膜型人 工肺 Platinum Cube NCVC シ リーズ

膜型人工肺を用いた経皮的心肺補助法(percutaneous cardiopulmonary support: PCPS)や ECMO (extracorporeal membrane oxygenation) は,重症呼吸循環不全患者への強力な治療法として,心臓外科領域に限らず,救命救急領域などにおいても広く普及しはじめている。しかしながら,これら新しい救命法や治療法が普及するにつれ,その長期使用や適用の拡大などに対するハードウェア整備の立ち後れが指摘されるようになってきた。

かかる問題に対し、われわれは、大日本インキ株式会社と共同開発をおこなってきた中空糸表面に 200 nm 以下の緻密層を形成し、ガス交換能にもすぐれた特殊ポリオレフィン膜を使用した膜型人工肺に、さらに T-NCVC コーティングを採用し、長期の耐久性および生体適合性にすぐれた次世代型膜型人工肺 Platinum Cube

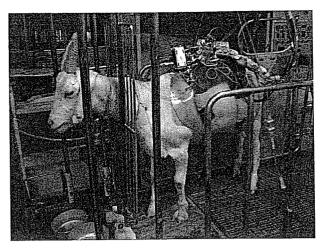


図 **○** T-NCVC コーティング PCPS システムの長期動物 実験風景

NCVC シリーズを完成させた(図⑥). また, この膜型人工肺 Platinum Cube NCVC 6000 を使用し, 回路全体にT-NCVC コーティングを施した次世代型 PCPS システムを開発し,成ヤギを用いた長期動物試験により,本システムの血液適合性および長期耐久性について検討をおこなった.

実験では成ヤギに対し、右心房脱血、頸動脈送血によ る静動脈バイパス術を施し、覚醒下において試験システ ムを最長 65 日間持続的に駆動させ, その血行動態, 血液, 血球成分の変化、および実験終了後におけるシステム内 での血栓形成状況について検討をおこなった(図録). な お、実験期間中の抗凝血療法はヘパリンを手術中のみ使 用し、術後の長期管理中には血圧モニター用ライン維持 を目的としたきわめて微量な投与をおこなうのみで実験 をおこなった.その結果,全例において実験期間中には, 膜型人工肺のガス交換能などの機能低下や血漿リークな ど異常所見は認められず,良好な状態で静動脈バイパス を維持することが可能であった。血液生化学的には、実 験期間中の賦活化血液凝固時間 (activated clotting time: ACT) は、術前値とほぼ変化せず、血小板数の軽 度の低下を認めたのみで、アンチトロンビンIII、フィブ リノーゲンおよびフィブリノーゲン・フィブリン分解産 物も最長2ヵ月まで著変は認められなかった. 実験終了 後の膜型人工肺の血栓形成状況は,そのケース辺縁部に 若干の血栓形成を認めたが、中空糸膜の層間内部にはほ

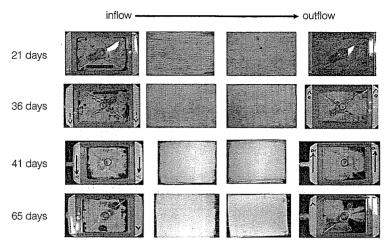


図
 長期動物実験後の T-NCVC コーティング膜型人工肺 抗凝血療法をおこなわない長期動物実験後においても、本人工肺には ケーシング周辺に血栓形成が認められのみであり、中空糸膜には血栓 の付着などは認められなかった。 (西中知博ら、2002<sup>4</sup>)より引用)

とんど認められなかった (図8).

以上より、われわれの開発した次世代型膜型人工肺Platinum Cube NCVC シリーズを組み入れ、回路全体にT-NCVC コーティングを施した PCPS システムは、抗凝血療法を不要とする持続的な長期的使用が可能であることが示された。また、本システムは長期に安定した血液適合性能を維持しうることから、従来のシステムでは適応できなかった、出血を伴う外傷や脳血管障害および長期心肺補助を必要とする種々の症例への適応拡大が見込まれ、従来の静動脈バイパスのみならず、低流量循環が必要な静脈一静脈および右房一肺動脈バイパスなどのアプローチ選択の多様化など、さまざまな病態ごとに適した循環および呼吸補助法に対応可能な次世代治療に適したシステムになりうると考えられた。

さらに、われわれは現在 Platinum Cube NCVC シリーズのなかでも最小モデルである Platinum Cube NCVC 2000 を組み入れた低灌流用 PCPS システムの開発をおこなっており、小児用あるいは新生児用 ECMO に最適なシステムの開発、製品化が期待されている<sup>7</sup>.

#### おわりに:今後の展望について

重症心不全ないし呼吸不全患者に対する人工臓器治療 の適用数は、機器やその材料の発達により安全性や耐久 性が向上し、年々増加傾向にある。また、傷害臓器の回復や移植(Bridge to Transplantation)を見据えた比較的短期の使用を目的とした適用から、ドナー不足による移植待機時間の延長や、心機能の回復を見込めない症例に対する恒久的な使用を目的とした Destination Therapyへの適用のための長期治療まで、その使用法は多岐にわたる傾向にある。かかる状況に対し、人工臓器の長期的な耐久性、および確かな安全性の向上を求める声は根強く、とくに血液との接触が不可避な循環器系人工臓器においては、長期使用の安全性を確保するため、抗血栓性や生体適合性の長期的な維持が重要な課題となっている。

われわれが開発した表面処理技術 T-NCVC コーティングは、ナノサーフェーステクノロジーを応用した新しいコンセプトに基づき、きわめて高い血液適合性と同時に長期耐久性や処理の簡便性を実現することに成功した新規技術である。これらの技術を統合して開発する、抗凝血療法不要の長期連続使用が可能な次世代型人工心臓や膜型人工肺は、従来の機器の最大の欠点であった血栓塞栓症の発生や抗凝血療法併用による致死性出血性臓器障害の発生を激減させ、外傷患者、脳血管障害既往患者および従来システムでは適応になりえなかった慢性呼吸循環不全患者の急性増悪時の短中期心肺補助に対する中長期補助も可能とするなど、その特性を十分に活用させた適用範囲、適用環境が飛躍的に拡大することが期待さ

れている。現在の研究では、T-NCVCコーティングが、 器材表面に接触する細胞の接着作用を著しく阻害する効果を有することが見出されているものの、この細胞接着 阻害作用は、従来提唱されていた作用機序とは異なる結果が多く認められていた。故に、T-NCVCコーティングの有する細胞接着抑制機序には、従来の抗血液凝固性機序とは異なった新しい機序が存在する可能性が想起され、かかる新機序を解明することによりT-NCVCコーティングの血液に対する適合性をより機能的に向上させることが可能になると考えられる。

また、本コーティングに使用されるへパリンは、生物製剤として人畜共通感染症に対するスクリーニングの必要性があり、その供給についても不安定な側面をもつことが問題として挙げられる。そのため、これからの次世代型の抗血栓法の開発には、T-NCVCコーティングの機能を損なわず、ヘパリン剤を合成高分子化合物に置き換えることが必要であり、かかる諸問題を早期に解決することは、さらに次世代型の生体適合性表面処理法を開発するための重要な課題と考えられる。

しかしながら、現段階において非常に優秀な成績を得ている T-NCVC コーティングをもってしても、人工臓器内に発生する血栓形成を完全に抑制することは非常に困難であり、Toyobo-NCVC VAS では、弁輪周囲部のように血栓形成に対し構造的に不利な部位への適用には限界があることも事実である。したがって、これからの人工臓器開発においては、ナノ単位で表面改変が可能なナノサーフェーステクノロジーと、構造学的および流体工学的な見地からマクロ構造を改良するマクロサーフェーステクノロジーを同時に見直すことが重要であり、ナノからマクロへ、マクロからナノへの技術の循環

が、より安全ですぐれた次世代型デバイス開発に必要であると考える.



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## The Significant Improvement of Survival Times and Pathological Parameters by Bioartificial Liver With Recombinant HepG2 in Porcine Liver Failure Model

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Key words: Bioartificial liver (BAL); HepG2; Ischemic liver failure; Porcine hepatocytes

#### INTRODUCTION

The bioartificial liver (BAL) was conceived as a support system providing liver function by using an artificial module with living hepatic parenchymal cells (2,4, 15). Most researchers use primary hepatocytes from pigs as the reactor cells, because 1) primary culture hepatocytes have a full range of hepatic functions, 2) porcine hepatocytes are much easier to obtain practically and ethically than human primary hepatocytes, and 3) porcine materials have already been utilized for several medical purposes, although their clinical use is still adventurous (16,20,24). However, the hepatic functions such as drug metabolism and ammonia removal are reduced under the culture condition, and BAL activity only lasts for 10-20 days. When hepatocytes have been cryopreserved, cell viability and functions, especially cell attachment to the culture matrix, markedly decrease. In addition, from a public health viewpoint, the potential risk of infection from porcine endogenous retrovirus applies not only to patients themselves, but also the public at large (21). Therefore, the BAL with primary porcine hepatocytes is not yet suitable as a medical apparatus, even under conditions of well-defined quality control.

When lined cells are used as bioreactor cells, the major problem is their decreased hepatic functions (7). Nevertheless, quality control is easier with these cells than with primary hepatocytes. In addition, advantages in use of lined cells are as follows: 1) indefinite growth, 2) feasibility of frozen storage and elimination of infectious agents, 3) a low ethical problem for cell preparation. The human hepatoblastoma cell line, HepG2, is one promising cell line for the bioreactor of the BAL because HepG2 maintain differentiated characteristics of normal parenchymal cells, such as drug-metabolizing activity and production of albumin and transferrin [(6) and our unpublished results]. Previously, the HepG2 subline, C3A, was examined for effectiveness as reactor cells of BAL or ELAD® (extracorporeal liver assist device) in an acetaminophen-intoxicated canine model and a clinical study was performed (5,22). Recently, the development of ELAD®, including phase I and II clinical study, was transferred to Vital Therapies, Co. Ltd (San Diego, CA). However, there was an unresolved problem, 874 ENOSAWA ET AL.

in that neither HepG2 nor C3A had ammonia removal activity (6).

We have added ammonia removal activity to HepG2 by transfecting the glutamine synthetase (GS) gene (9). GS is localized in hepatic parenchymal cells aligned around the central vein and catalyzes an accessory pathway of ammonia removal by synthesizing glutamine from glutamate and ammonia. We have previously shown that GS-transfected HepG2 (GS-HepG2) removed ammonia in the culture medium with 1/7 of the activity of porcine hepatocytes (9,19). In this report, we applied the BAL with GS-HepG2 to pigs with ischemic liver failure, to observe the survival time and other parameters related to hepatic function. Our standardized simple model of liver failure using pigs enabled a large number of experiments with highly reproducible results (18). We also configured a novel criterion in survival time, active survival time in the previous report (18). Active survival time is defined as the time until when the systolic pressure becomes less than 50 mmHg, while gross survival time is until the cessation of heart beat. In this report, we analyzed all survival data with the concept of active survival time. These two methodological improvements enabled the comparison of various experimental conditions, including the present conventional treatment of plasma pheresis, resulting in the discovery of the significant prolongation of survival time with the recombinant HepG2 BAL treatment and decreased incidence of brain pressure rise.

#### MATERIALS AND METHODS

Bioreactor Cells and Culture System

We have previously described the method for establishing the bioreactor cells, GS-HepG2 (9,19). Briefly, the hamster GS gene was transfected to HepG2 (RIKEN Cell Bank, Tsukuba, Ibaraki, Japan). The transfected cells were cultured in the presence of methionine sulfoximine to amplify the transfected GS gene. The GS-HepG2 ( $2 \times 10^8$  cells) that were subcultured in 20 culture flasks (150 cm<sup>2</sup>, 430824, Corning, NY, USA) were inoculated into the circulatory flow bioreactor (U.S. Patent 5270207, 1993) and cultured as shown in Figure 1. When the cells grew to stationary phase (total cell number;  $3.5-4.1 \times 10^9$ ) as indicated by the glucose consumption rate, in vivo estimation of the BAL was carried out. As one of the control experiments, a BAL with wildtype HepG2 cells was prepared, as mentioned above, for the GS-HepG2 BAL. A BAL with one batch of reactor culture was used for a series of four in vivo experiments at 1-week intervals. Immediately after finishing the series, the cells were harvested from the culture matrix to determine cell number and viability, using crystal violet and trypan blue solution (9).

Animals and Hepatic Failure Model

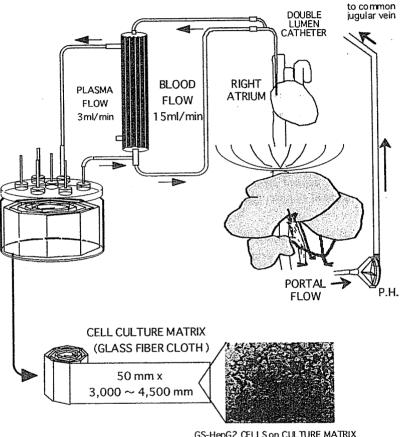
Domestic piglets cross-bred with Large-Yorkshire, Landrace, and Dulroc (approximately 25 kg, 2-3 months old) were purchased from Kidokoro farm (Atsugi, Kanagawa, Japan) and kept in our animal facility prior to the operation. The animals were used within 2 days of transportation. All experimental procedures were performed according to the institutional animal ethics guidelines, based on the guidelines of the National Institute of Health, USA (23). Ischemic liver failure surgical procedure has previously been described in detail (18). Briefly, after the portal flow was by-passed to the jugular vein with a centrifugal blood pump (HPM-15, Nikkisou, Tokyo, Japan), the portal vein, common hepatic artery, and common bile duct were ligated. Inorganic salt solution (Sublood B, Fusou Pharmaceuticals, Osaka, Japan) containing 5% glucose was continuously supplied after the operation. The concentration of inhalation anesthetic, tidal volume, oxygen concentration, the rate of infusion, and the addition of glucose, heparin, and sodium bicarbonate were adjusted as expedient, in accordance with our previous report (18). No vasopressor was used in the experiment.

#### Treatment With BAL and Plasma Pheresis

Three hours after total liver ischemia, the BAL treatment was started, as described in Figure 1. Blood access was performed using a double lumen catheter (14 gauge, Medicut UK-II Catheter Kit®, TYCO Healthcare, Mansfield, MA, USA) inserted into the right atrium via the right jugular vein. Outflow of blood was led to a hemodialysis console (JUN-500, Ube Medical, Tokyo, Japan) at 15 ml/min, and plasma was separated at a rate of 3 ml/min by hollow fiber column (PP-03, Ube Medical, Tokyo, Japan). The plasma was passed through the BAL with or without reactor cells and returned to extracorporeal circulation. Extracorporeal volume (200 ml in the tube and 550 ml in the bioreactor including hollow fiber ventilation unit) was primed with Sublood B. During the first 3 h from the beginning of BAL treatment, the animals were transfused with 500 ml of freeze-stored pig plasma at a rate of 167 ml/h.

In the group treated with plasma pheresis, we connected two hemodialysis consoles serially: one for plasma separation and the other for hemodiafiltration (12). The plasma separation flow rate was the same as described above. The supplementation with normal pig plasma was done at an equivalent rate during the first 6 h. Total amount of exchanged plasma was approximately 1000 ml, almost equal to the total body plasma of a piglet. Hemodiafiltration was performed with the second console, using hollow fiber column (FH-66D, Gambro, Hechingen, Germany). Flow rates were 15 ml/min for blood, 100 ml/min for dialysis fluid, 150 ml/min for fil-

BAL INTERFACE (PLASMA SEPARATOR) ANIMAL MODEL (PIG WITH ISCHEMIC LIVER FAILURE)



GS-HepG2 ŒLLS on CULTURE MATRIX on Culture day 109. (Scanning Electron Microscopy)

Figure 1. Schematic illustration of connection of BAL and hepatic failure pig. Separated plasma was flown into the BAL. Separated plasma was flown into the BAL and returned to blood flow (P.H.: pump head of centrifugal blood pump). When the cells grew to stationary phase (total cell number 3.5–4.1 × 10°), the BAL experiment was carried out. A BAL with one batch of reactor culture was used for a series of four experiments at 1-week intervals. Domestic piglets (approximately 25 kg, 2–3 months old) were used. After the portal flow was by-passed to the jugular vein with a centrifugal blood pump, the portal vein, common hepatic artery, and common bile duct were ligated. Three hours after total liver ischemia, the BAL treatment was started. Blood access was performed using a double lumen catheter inserted into the right atrium via the right jugular vein. Outflow of blood was led to a hemodialysis console at 15 ml/min, and plasma was separated at a rate of 3 ml/min by hollow fiber column. The plasma was passed through the BAL and returned to extracorporeal circulation. Extracorporeal volume (200 ml in the tube and 550 ml in the bioreactor including hollow fiber ventilation unit) was primed with Sublood B. During the first 3 h from the beginning of BAL treatment, the animals were transfused with 500 ml of freeze-stored pig plasma at a rate of 167 ml/h.

trate, and 50 ml/min for infusion. Inorganic solution, Sublood B, was used for dialysis fluid and infusion. The sustentation protocol was the same as that for nontreatment, cell-free BAL, and BAL treatment according to the method described in the previous report (18).

Monitoring Physiological Conditions and Determining Survival Time

Physiological indices such as heart rate, blood pressure, and intracranial pressure were continuously recorded using a bedside monitor (Model66S, Hewlett Packard, Palo Alto, CA, USA). Blood samples were taken just prior to the liver ischemia and at 3-h intervals throughout the experiment. The endpoint of survival for the animal was taken as the time either when systolic pressure fell below 50 mmHg (referred to as "active survival time") or when the heart beat stopped (referred as "gross survival time") as was defined previously (18). The survival hours are expressed as mean and standard deviation.

Analysis of Blood Ammonia and Coagulation Indices

Activated clotting time (ACT) was determined by Hemochron 401® (International Technodyne, Edison, NJ, USA), and activated partial thromboplastin time (APTT) was determined with the assay protocol for human coagulation indices as described elsewhere (1).

#### Statistical Analysis

Dunnet type multiple comparison with Bonferroni adjustment in the Peto mortality-prevalence test for differences in active survival times (Table 1), the chi-square test for incidence of brain pressure increase (Table 2), and the Mann-Whitney U test for blood coagulation indices (Fig. 3) were used. All tests were two-tailed and performed using PC-SAS (PC/SAS, SAS/BASE, SAS/STAT Software, Version 8.2, SAS Institute Inc., Cary, NC, USA).

#### RESULTS

Ammonia Removal Activity of GS-HepG2 BAL

GS-HepG2 cells grew to the stationary phase, as judged by glucose consumption rate, 40-60 days after their inoculation into the circulatory flow bioreactor. Glucose consumption increased from 0.47 g/day at day 7 to  $1.72 \pm 0.12$  g/day in the stationary phase (n=4, day 40-60). Although the glucose consumption rates of GS-HepG2 and wild-type HepG2 were similar, ammonia removal activity was detected only in GS-HepG2. The rate was  $36 \mu$ mol/h from culture medium and hepatic failure plasma, both of which contained 3 mmol/L ammonia. The rate of ammonia decrease by GS-HepG2 was approximately 15% of primary porcine hepatocytes (in preliminary data). In contrast, with wild-type HepG2, ammonia level progressively increased at a rate of 25

 $\mu$ mol/h. The final cell numbers of the two batches of bioreactor culture of GS-HepG2 were  $3.5 \times 10^9$  and  $4.1 \times 10^9$ . Those of wild-type HepG2 were  $3.6 \times 10^9$  and  $3.8 \times 10^9$ . The cell density was  $1 \times 10^7$  cells/cm³ in the bioreactor and  $3.8 \times 10^6$  cells/cm² on the glass fiber cell matrix. After the BAL treatment began, the blood ammonia levels in the GS-HepG2 group were kept lower than that in the cell-free control, although there was no statistical significance (data not shown).

#### Survival Times of Pigs

Table 1 shows the overall result of active and gross survival times in this experiment. While there are nontreated and cell-free BAL-treated groups as controls, the proper control to compare the BAL efficacy is cell-free BAL group [8.53  $\pm$  2.52 h (active survival time) and 11.98  $\pm$  5.28 h (gross survival time)]. Plasma pheresis treatment that was clinically performed as hepatic support showed no prolongation of the survival [7.19  $\pm$  3.49 h (active survival time) and 9.47  $\pm$  4.12 h (gross survival time)]. Among the five experimental groups, the survival time was longest in the group treated with BAL

**Table 1.** Active Survival Time of Pigs With Ischemic Hepatic Failure

	Active Survival Time (h)	Gross Survival Time (h)			
Group (n)					
			Nontreated (8)	7.61 ± 2.56*	$8.18 \pm 2.58$ §
			Cell free (9)	$8.53 \pm 2.52 \dagger$	$11.98 \pm 5.28$
PE + CHDF(8)	$7.19 \pm 3.49 \ddagger$	9.47 ± 4.12#			
W-HepG2 (8)	$9.78 \pm 4.31$	$10.54 \pm 4.23$			
GS-HepG2 (8)	$14.52 \pm 5.28$	$16.38 \pm 6.22$			

Values are mean  $\pm$  SD. Data of nontreated group are from our previous report (12). Groups abbreviations: Cell free, treated with cell-free BAL; PE + CHDF, treated with plasma exchange and continuous hemodiafiltration; W-HepG2, treated with BAL of wild-type HepG2; GS-HepG2, treated with BAL of GS-HepG2. Active survival time is defined as the time from completion of hepatic total ischemia to the time when systolic blood pressure was decreased under 50 mmHg. Individual data were: nontreated (4.60, 6.00, 6.00, 6.25, 8.17, 8.20, 8.75, 12.90 h), cell free (4.52, 5.87, 7.10, 7.90, 8.60, 9.32, 10.07, 10.67, 12.75 h), PE + CHDF (4.70, 5.25, 5.53, 5.60, 6.00, 6.20, 9.05, 15.20 h), W-HepG2 (5.53, 6.43, 6.90, 7.42, 8.03, 11.73, 16.03, 16.20 h), GS-HepG2 (4.63, 10.03, 12.83, 15.40, 15.43, 18.23, 19.67, 19.92 h). Gross survival time is defined as the time from completion of hepatic total ischemia to the time of heart beat arrest. Individual data were nontreated (4.65, 6.10, 6.32, 8.40, 8.72, 8.95, 9.20, 13.13 h), cell free (5.00, 9.00, 9.27, 10.08, 10.75, 11.05, 11.28, 20.63, 20.73 h), PE + CHDF (5.18, 6.57, 6.77, 7.17, 7.90, 11.00, 15.37, 15.80 h), W-HepG2 (5.53, 6.43, 8.32, 8.38, 10.70, 11.95, 16.20, 16.83 h), GS-HepG2 (5.83, 12.12, 13.12, 16.23, 16.78, 20.07, 20.63, 26.33 h). Statistical significance (p < 0.05) was determined by Dunnet type multiple comparison with Bonferroni adjustment.

- \*p = 0.009, GS-HepG2 versus nontreatment.
- †p = 0.032, GS-HepG2 versus cell free.
- $\ddagger p = 0.002$ , GS-HepG2 versus PE + CHDF.
- \$p = 0.009, GS-HepG2 versus nontreated.
- #p = 0.036, GS-HepG2 versus PE + CHDF.

containing GS-HepG2 cells  $[14.52 \pm 5.28 \text{ h} \text{ (active survival time)}]$  and  $16.38 \pm 6.22 \text{ h} \text{ (gross survival time)}]$ . The p values on active survival times between this group and the groups with nontreatment, cell-free BAL, and plasma pheresis were 0.009, 0.032, and 0.002. Survival time with GS-HepG2 BAL was 1.5 times longer than with wild-type HepG2 BAL  $[9.78 \pm 4.31 \text{ h} \text{ (active survival time)}]$  and  $10.54 \pm 4.23 \text{ h} \text{ (gross survival time)}]$ , although there was no significance between these groups (p = 0.189 and 0.162, respectively).

Whereas the gross survival time of GS-HepG2 BAL was the longest, the statistical significance was only detectable toward nontreatment and plasma pheresis groups (p = 0.007 and 0.036, respectively). Because the proper control of BAL treatment group is cell-free BAL treatment, the effectiveness of BAL was not confirmed as far as the survival endpoint was taken as the cessation of heart beat.

The difference between active and gross survival times ranged from 0.48 to 9.96 h (3.44  $\pm$  3.25 h, mean  $\pm$  SD) in the cell-free BAL group, and from 0.29 to 6.41 h in the GS-HepG2 BAL group (1.87  $\pm$  1.92 h), indicating that the terminal stage, with low systolic blood pressure, was short in the GS-HepG2 BAL-treated group.

When survival data were compared between the BAL-treated groups (GS-HepG2 BAL and wild-type HepG2 BAL) and the others (nontreatment, cell-free BAL, and plasma exchange), active survival time was significantly prolonged in the former groups (12.05  $\pm$  5.37 h vs. 7.81  $\pm$  2.91 h, p=0.0187). To detect the unknown but stable effect of cellular biological activities, the cell-free and cell-treated data are compared below.

#### Incidence of Increased Brain Pressure

There were two types of brain pressure profiles during the progression of hepatic failure: increased type and flat type (Fig. 2). In the increased type, systolic blood pressure dropped markedly just after the peak of brain pressure, followed by a steady low-level state. Half of the cases without cell treatment were the increased type (Table 2). In contrast, only 2 out of 16 cases in the cell treatment group were the increased type (p = 0.034 by chi-square test).

#### Improvement in Blood Coagulation Indices

When blood coagulation indices of surviving animals at 12 h after liver ischemia were compared between the BAL-treated groups and the others, there was significant improvement in APTT and ACT (Fig. 3). However, hepaplastin and factor VII decreased similarly, both in the cell-treated and the other groups (data not shown).

#### DISCUSSION

We have examined the efficacy of recombinant GS-HepG2 as BAL reactor cells (8,17). While the previous

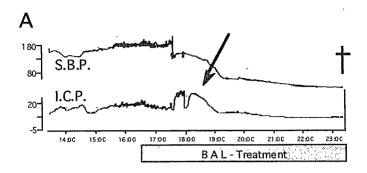
works indicated a sign of improvements in physiological indices, the present report demonstrated statistically significant results on survival time, incidence of increased brain pressure by introduction of the concept of "active survival time." and accumulation of experiments.

As we mentioned in the previous report (18), indeed the survival time of animals is one critical index of BAL efficacy, yet the cessation of heart beat is not a proper endpoint. Because the aim of BAL treatment is to rescue patients, not just prolongation of life, the endpoint should be set before the point of no return. According to our careful observation and detailed analysis, the pigs with systolic pressure over 50 mmHg are able to respond to the bolus transfusion of glucose to increase the pressure (18). Therefore, we embrace the concept of active survival time to estimate the BAL efficacy.

Ammonia is a classical endogenous toxin that may be responsible for the etiology of hepatic coma. Because ammonia removal activity is intrinsic to hepatocytes, this activity is also essential in BAL function. Our original purpose was to remove ammonia from hepatic failure plasma using the BAL with HepG2-supplemented ammonia removal activity. Although hemodialysis can remove ammonia in blood, other low molecular substances are also dialyzed, regardless of their physiological importance. Using the porcine model, we performed the BAL treatment in a closed extracorporeal circuit, obtaining two important results that conventional plasma pheresis does not achieve (i.e., the support of multiple liver functions and the preservation of potentially beneficial substances in blood circulation).

By large-scale culture of GS-HepG2, we obtained ammonia removal activity at 36 µmol/h, which is 1/4 of the total ammonia increase in the pig (140 µmol/h), as calculated from the previous report (19). The mean blood level was kept lower in the GS-HepG2 BAL group than in the wild-type HepG2 BAL group, although there was no statistical significance (8). Nevertheless, active survival time was prolonged significantly in the GS-HepG2-treated group. In addition, when the experimental groups were divided into the cell treatment group and others, the former exhibited significantly increased survival times. Together with the reduction in the incidence of increased brain pressure, the cell-containing BAL improved hepatic failure at the end stage. The reason for this improvement is not clear at present, but may be partly due to a removal of cytokines by the cells in the BAL.

Interestingly, an improvement was also seen in the blood coagulation indices, APTT and ACT (8,17). We hypothesize that the BAL suppressed endogenous consumption of coagulation factors by an unknown mechanism. Although synthetic activity of proteins, such as transferrin and albumin, is low in HepG2 (our preliminary data), certain physiological factors may be respon-



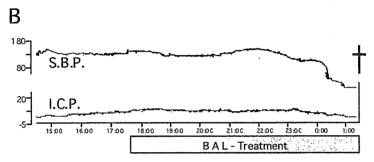


Figure 2. Typical two patterns of brain pressure change. (A) Increased brain pressure (arrow) was observed prior to the rapid decline of systolic blood pressure. (B) Brain pressure was almost unchanged during the experiment. S.B.P.: systolic blood pressure; I.C.P.: intracranial pressure. †Time of cardiac arrest.

sible for prolongation of survival time. Actually, we determined that the culture supernatant of GS-HepG2 induced rat hepatocyte proliferation in vitro and in vivo (11).

The cell numbers required in the BAL to support severe hepatic failure is still unclear in the present experimental model. One enigma in the research of BAL and cell transplantation is discrepancy of cell ability and the efficacy. In this report, too, the calculated efficacy of the BAL is too low to support the whole animal body, but significant prolongation and decreased incidence of brain pressure rise was observed. A minimum requirement for survival was reported to be 10% of total liver weight after extensive partial hepatectomy in rats (13),

Table 2. Decrease of Cases With Rise of Intracranial Pressure

Intracranial Pressure	BAL Treated	Others
Increase No increase*	2 14	11 14

BAL treated: groups treated with GS-HepG2 and wild-type HepG2 BAL. Others: Nontreated control and groups treated with cell-free BAL and plasma exchange.

in which model, however, the remnant hepatocytes were almost intact. For BAL usage, a greater number of hepatocytes may be necessary, because the cell activity is decreased by their isolation and the culture process. In the hepatocyte transplantation model in rats, the effective number of cells ranged from  $4\times10^6$  to  $7\times10^7$ , which was estimated to be 0.2–3.5% of the total parenchymal cells in the normal liver [reviewed in (3)]. Moreover, nonhepatic cells, such as splenic lymphocytes and bone marrow cells, were reported to be effective in the treatment of hepatic failure (14). Although the mechanism for this is not completely understood, normalization of the cytokine network may be involved. Further study, including our own, will be necessary to elucidate these phenomena.

The lined cells established from either tumor tissue or immortalized normal cells possess an intrinsic risk of virulence by oncogenes. In this experiment, we returned the plasma directly to host circulation after incubating in the BAL. For clinical application, a filtration system or other device to eliminate the risk must be considered. The ideal source of bioreactor cells for BAL would be hepatic stem cells, which have the ability to grow and differentiate. Because most BAL modules are designed to integrate nondividing hepatic parenchymal cells, long-term survival of the reactor cells is not expected.

<sup>\*</sup>p = 0.034 by chi square test.

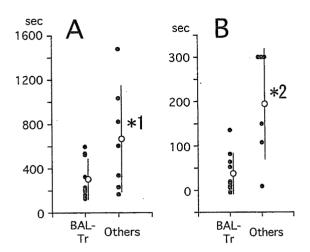


Figure 3. Comparison of blood coagulation indices between BAL treatment and the other groups. (A) Activated clotting time (ACT), \*1: p = 0.040. (B) Activated partial thromboplastin time (APTT), \*2: p = 0.017. Closed circles indicate individual data of surviving animals 12 h after hepatic ischemia. Open circle and bar indicate mean  $\pm$  SD. Statistical significance was determined by Mann-Whitney U test.

From this point of view, our circulatory flow bioreactor is suitable for long-term culture of growing cells, including hepatic stem cells.

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#### Double-Compartment Cell Culture Apparatus: Construction and Biochemical Evaluation for Bioartificial Liver Support

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Functional demands on a bioartificial liver support (BAL) device are not limited to biosynthetic activities, but must also encompass metabolic removal of potentially toxic substances. For most BALs, however, the concept and design are exclusively directed to biosynthetic support. To add the ability to metabolize and remove toxic substances, we designed a double-compartment cell culture apparatus (DCCA). Two compartments are separated from each other by a compact epithelial cell sheet spread over a synthetic microporous membrane. When a renal proximal convoluted tubular cell line that had been transduced with the human multidrug-resistant (MDR) gene, PCTL-MDR, was introduced into one of the compartments (hereafter referred to as the "inner" compartment) of the DCCA, a compact cellular monolayer was formed on the membrane. Ammonium ions passed across the membrane, but glucose and its metabolite lactate could not, indicating that the DCCA allowed selective transportation of cellular metabolites. In addition to PCTL-MDR, HepG2, a cell line of hepatic-origin, transduced with CYP3A4 (designated GS-3A4-HepG2), was seeded on the opposite side of the membrane, and the metabolism and transportation of lidocaine were studied. The lidocaine metabolite, monoethylglycinexylidide, was detected in the inner compartment across the PCTL-MDR cell layered membrane, indicating that metabolism and the selective transportation of metabolites between the two compartments occurred by cooperation of renal and hepatic cells. These results suggest that this type of DCCA represents a novel BAL that possesses biotransporting activities, as well as biosynthetic and metabolic activities.

Key words: Bioartificial liver support; Double-compartment cell culture apparatus; Toxic substance removal; Biotransport activity

#### INTRODUCTION

Progress in modern biotechnology and medicine enables artificial devices to support patients at the end stage of organ failure (12,17). One major application of these devices is the support of liver function. There are two concepts in extracorporeal artificial liver support: the nonbiological approach or the cell-based hybrid approach. The former has been developed as plasmapheresis (9) and the latter as bioartificial liver support (BAL) (2,16). Over the past few years, some cell-based BALs succeeded in providing life support for patients with fulminant hepatic failure waiting for liver transplantation (2,4,13,16). Moreover, temporary support with a BAL may allow time for the patient's own liver to regenerate without need for transplantation.

A typical type of BAL is composed of a hollow fiber module in which hepatocytes are packed either outside or inside the hollow fiber tubules, and the patient's plasma or blood interacts with the cells through the hollow fiber membrane (4,16). In another model, hepatocytes are cultured on support matrices such as small beads or membranes, and patient plasma is applied directly (2,11,15). Previously, we developed a BAL of fixed bed perfusion reactor type, which essentially belongs to the latter model, and succeeded in extending the survival time of pigs with ischemic liver failure (7).

The above two BAL models carry out hepatic biosynthesis and metabolism, but cannot actively transport toxic substances. During the development of our BAL, we noticed that hepatocytes alone are not sufficient for achieving biological transportation. Therefore, in addition to

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hepatocytes, we chose a cell line of kidney proximal convoluted tubule origin, PCTL-MDR, to perform metabolism and active transportation tests. The cell line, PTCL, was first established from rabbit kidney proximal cells by transduction of SV40T antigen, and further transduced with multidrug-resistant (MDR) gene to increase anion transport activity, and therefore termed PCTL-MDR (19). In a small-scale experiment, the monolayer membrane of PTCL cells successfully transported a model toxic substrate, digoxin, and hydroxytestosterone, which was produced by recombinant HepG2 (5,6). To develop a preclinical scale module that is applicable for experimental animals such as rabbits and pigs, we designed and constructed a double-compartment cell culture apparatus (DCCA) with a membrane separating the two compartments on which actively transporting cells are layered. This communication describes the construction and functional characteristics of such a DCCA and discusses prospects for use of this novel module design.

#### MATERIALS AND METHODS

Brief Description of the Double-Compartment Cell Culture Apparatus (DCCA) and Circulation System

The body of the DCCA consists of a pair of 5-mmthick glass plates (150 × 250 mm) and a pair of sizematched 3-mm-thick silicon molds with a square window (110 × 210 mm) as shown in Figure 1. Expanded polytetrafluoro-ethylene (ePTFE) microporous membrane (Fluoropore, FP100, Sumitomo Electric Industry, Osaka, Japan) was set between the two silicon molds so that it divided the inner space into two compartments in the middle. The average pore size of the ePTFE membrane was 1 µm and thickness of 75 µm. There was a conformable zigzag flow pass (32.5 mm width) in each compartment. The volume and area of flow pass were 64.5 cm<sup>3</sup> and 215 cm<sup>2</sup>, respectively. These components (i.e., glass plates, silicon molds, and an ePTFE membrane) were held tightly together in aluminum frames with clamps to form the DCCA. For autoclaving, they were put together loosely, and tightened after cooling.

The DCCA possesses a pair of outlets and inlets for each compartment (Fig. 2). Medium is circulated independently through each compartment by way of separate reservoir bottles (500 ml each), using a peristaltic pump (Master Flex L/S 7520-10) with a 7012-20 type pump head (Cole-Parmer Ins., IL, USA). Reservoir bottles were supplied with 5% CO<sub>2</sub>/95% O<sub>2</sub> gas continuously to adjust medium pH to 7.2. Each circulation line has a cell inoculation port and two air-trap chambers. The entire system, including reservoir bottles, can be placed in an incubator at 37°C. DCCA were placed vertically to avoid accumulation of air bubbles, except at the time of cell inoculation.

Flow Control and Membrane Permeability Test

After DCCA assembly, a solution of 0.15 mol/L NaCl was constantly circulated at the rate of 10 ml/min. To visualize medium flow, 1 ml of blue dextran (10 mg/ml, Sigma) was added directly to the circulation medium through the inlet tube.

To determine the diffusion rate of small molecules across the cell-free ePTFE membrane in the DCCA, a test solution (0.15 mol/L NaCl containing either 0.2 mol/L calcium lactate, 1.0 mmol/L ammonium sulfate, or 17.5 mmol/L glucose) was circulated in one of the two circuits at the rate of 10 ml/min. NaCl solution flow in the other compartment was at the same rate and samples were collected from each reservoir at 4-h intervals. Time-dependent change of lactate concentration was determined using Lactate Pro Test Strip (ARKRAY Inc, Kyoto, Japan), that of ammonium ion concentration by using an AMICHECK Meter (ARKRAY Inc), and of glucose concentration using the anthrone-sulfuric acid method (3). Diffusion rates for lactate, ammonium, and glucose were calculated from these values.

#### Cell Culture Experiments

Before inoculation into the apparatus, cells were grown in 175-cm² culture flasks with a mixture (1:1) of Dulbecco's modified Eagle's medium and Ham's nutrient mixture F-12 (DMEM/F12 medium, Invitrogen, Carlsbad, CA, USA), supplemented with 5% fetal bovine serum (Invitrogen). GS-3A4-HepG2 and PCTL-MDR cells were cultured in the presence of 200 μg/ml Zeocin<sup>TM</sup> (R250-01, Invitrogen), or 40 μg/ml neomycin (Sigma, St. Louis, MO, USA), respectively. Cells at the subconfluent stage were harvested with 0.25% trypsin (15090-046, Invitrogen) for inoculation.

The sterilized DCCA was first filled with 95% ethanol to remove micro air bubbles in the ePTFE membrane. It was washed with phosphate-buffered saline and then filled with DMEM/F12 culture medium containing 5% fetal bovine serum.

Two different cell lines were inoculated successively on the opposite sides of the ePTFE membrane in a DCCA placed horizontally. First,  $1.0 \times 10^8$  kidney-derived PCTL-MDR cells in 100 ml were introduced into one side of the compartment through the circulation system using a peristaltic pump. After the inoculation, the apparatus was gently shaken for 5 min to allow the cells to spread evenly over the membrane. The apparatus was kept static for 1 h and medium circulation started at a flow rate of 1 ml/min for 3 h. The circulation rate was raised to 5 ml/min for an additional 21 h. Next, the DCCA was turned upside down, and  $1.0 \times 10^8$  GS-3A4-HepG2 cells were inoculated into the other compartment using the same procedure as for PCTL-MDR. Circula-

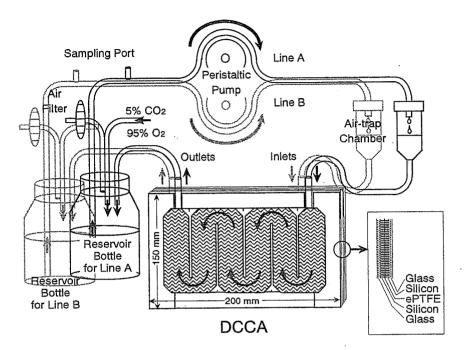


Figure 1. Schematic illustration of double-compartment cell culture apparatus (DCCA) and circulation system. A pair of symmetric culture chambers with zigzag flow path is formed on each side by piling up a pair of silicon molds and glass plates as shown in cross section (inset). The chambers were divided by an expanded polytetrafluoro-ethylene (ePTFE) membrane in the middle. Each chamber is supplied with medium through an independent line, Line A and B. The volume and area of flow pass were 64.5 cm³ and 215 cm², respectively.

tion of medium on the PCTL-MDR side was stopped during the second inoculation. Twenty-four hours thereafter, the apparatus was placed vertically and medium flow started on both sides (5 ml/min). Hereafter, the ePTFE membrane side on which PCTL-MDR cells were attached is referred to as the outer side, and the other side on which GS-3A4-HepG2 cells were attached as the inner side. Concomitantly, the compartment and the circulation of the outer side is referred to as the outer compartment and outer circuit, and those of the inner side as the inner compartment and inner circuit, respec-

tively. According to preliminary experiments,  $1.0\times10^8$  cells of PTCL-MDR reached confluence after 3 days of incubation.

During the culture period, unless otherwise stated, a medium reservoir bottle was changed every other day and a new bottle with 500 ml fresh medium substituted. Samples (5 ml) were taken from the two reservoir bottles at the times indicated, and stored frozen at  $-20^{\circ}$ C until HPLC analysis. In some experiments, lidocaine (final concentraton, 100  $\mu$ mol/L) (Alexis Biochemicals, Montreal, Canada) was added as a test substance to in-

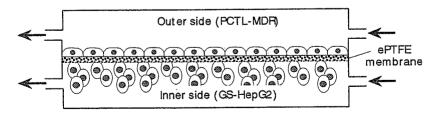


Figure 2. Cross section of DCCA. The inside of the vessel is divided by the ePTFE membrane and PCTL-MDR and GS-HepG2 cells are cultured on opposite sides. The PCTL-MDR side and GS-HepG2 side are termed outer and inner side, respectively.

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vestigate its metabolism and transportation across the membrane.

#### **HPLC** Analysis

Lidocaine and its metabolites in the culture medium were analyzed by a C18 reverse-phase column (particle size 5 µm, internal diameter 4.6 × 150 mm) (Inertsil ODS-3V, GL Sciences, Tokyo, Japan), using an HPLC system (Model 805, Waters, MA, USA). Prior to HPLC analysis, 2 ml of the medium was partially purified with a Sep-Pak Plus (Waters Corp., Milford, MA, USA), and 25 ul of the sample thus obtained applied to the column. Samples were eluted with 15% acetonitrile in 20 mmol/ L NaClO<sub>4</sub> solution (pH 2.5) at a flow rate of 2.0 ml/min at 40°C, and lidocaine and its metabolites detected at a wavelength of 205 nm (Type L-4000 UV detector, Hitachi, Tokyo, Japan). The authentic standard of lidocaine major metabolite, monoethylglycinexylidide (MEGX), was a generous gift from Astra Pharmaceuticals (Wayne, PA, USA).

#### RESULTS

#### Examination of Medium Flow

After the initial DCCA conception and design, several prototypes were constructed and tested. Improvements were mainly carried out on the shape of flow pass to remove air bubbles and to smooth medium flow. To remove air bubbles, inlet and outlet ports were changed from single tube form to branched tube form. To obtain a smoother flow, the shape of the corner of the compartment was changed from rectangular to trapezoidal (Fig. 3A). Although medium still flowed slightly faster in the middle of the stream, no dead space was now seen at any place in the compartment (Fig. 3B).

#### Passive Diffusion Across Cell-Free Membranes

As shown in Figure 4, the concentration of lactate achieved equilibrium between the two compartments by 28 h and ammonium and glucose by 20 h. Thus, the passive diffusion rate, P, was calculated from the time needed for the difference in metabolite concentration between the two compartments to be reduced by half,  $t_{1/2}$ ; the surface area of the membrane, S; and the volume of reservoir, V; using the following equation:  $P = \ln(1/2) \times V/S \times t_{1/2}$ . It was calculated to be  $5.1 \times 10^{-4}$ ,  $5.0 \times 10^{-5}$ , and  $8.5 \times 10^{-5}$  cm/s, respectively, for lactate, ammonia, and glucose.

#### Cell-Mediated Metabolism and Transport

When  $1.0 \times 10^8$  PCTL-MDR cells were seeded on the outer side of the ePTFE membrane, a tight monolayer was formed in 3 days. Fresh growth medium was replenished in the circulation units, and the concentrations of lactate ions, glucose, and ammonium ions were deter-

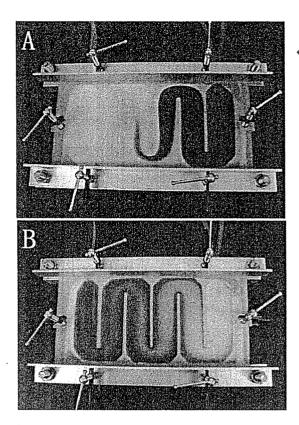


Figure 3. Examination of medium flow by blue dextran solution. One milliliter of blue dextran (10 mg/ml, Sigma) was added directly to a constant flow of 0.15 mol/L NaCl at a rate of 10 ml/min through an inlet tube. The time interval between (A) and (B) was 1 min.

mined every 12 h for the subsequent 7 days of constant circulation. The initial concentrations of lactate ions in both compartments were 0.8 mmol/L (Fig. 5A). After medium circulation began, the concentration level in the inner circuit (HepG2 site) was maintained around 0.8 mmol/L throughout the circulation period. On the other hand, the concentration in the outer circuit (PCTL site) increased steadily and reached 11.0 mmol/L at the end of the 7 days.

The ammonium concentration in the outer circulation was virtually unchanged and the level was maintained at between 4 and 5 mg/dl (mean  $\pm$  SD, 4.35  $\pm$  0.22 mg/dl) (Fig. 5B). In contrast, the level in the inner circulation medium decreased steadily from 4.6 mgN/dl to 2.7 mgN/dl during the 7 days.

The concentration of glucose in the outer circuit decreased steadily during the 7 days of circulation from 3.0 mg/L to 2.0 mg/L, while it was maintained in the inner circuit at approximately 3.2 mg/L (Fig. 5C).